

SIMSCI - Problem Descriptive Information

UDM Range Help

Project Identifier:

Problem Identifier:

User Name:

Site:

Print Report Date Based on:

☒ Problem Execution Date

☐ Date:

Problem Description

OK Cancel

Enter project name



SIMSCI - Default Units of Measure for Problem Data Input

UOM Range Help

Basis: English

Initialize from UOM Library...

Default Units of Measure for Problem Data Input

Temperature:	Fahrenheit	Energy:	British Thermal Unit
Pressure:	Pound/inch ² (abs)	Duty:	Energy/Time
Time:	Hour	Work:	Horsepower
Weight (wt.):	Pound	Length:	Foot
Liquid Volume:	Foot ³	Fine Length:	Inch
Vapor Volume:	Foot ³	Heat Trans. Coefficient:	BTU/hour-foot ² -F
Specific Liquid Volume:	Liquid volume/Molar wt.	Fouling Coefficient:	Hour-foot ² -F/BTU
Specific Vapor Volume:	Vapor volume/Molar wt.	Viscosity:	Centipoise
Liquid Density:	Weight/Liquid volume	Kinematic Viscosity:	Centistoke
Vapor Density:	Weight/Vapor volume	Thermal Conductivity:	BTU/hour-foot-F
Petroleum Density:	API gravity	Surface Tension:	Dyne/centimeter
Pressure Gauge Basis:	14.696 psia		

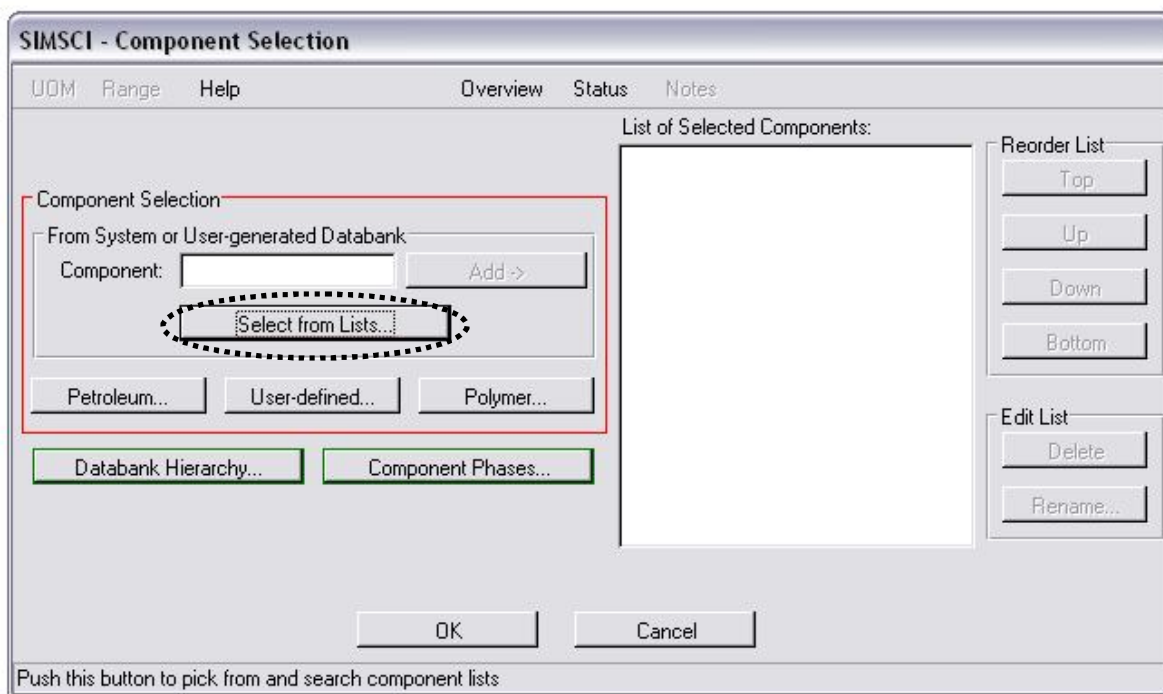
Standard Vapor Conditions...

TVP and RVP Conditions...

OK

Cancel

Exit the window after saving all data



PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

Summary Report X 100

PFD

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

Component Selection - List/Search

UGM Range Help

Component Family:

- Most Commonly Used
- Hydrocarbon Lightends
- All Components - PROCESS Bank
- All Components - SIMSCI Bank
- Acids
- Additional Electrolyte Components

Sort/Search by:

- ☒ Full Name
- ☐ SIMSCI Name/Alias
- ☐ Chemical Formula

Match:

- ☒ Initial String
- ☐ Embedded Substring

Search String: Search

Component Full Name:	SIMSCI Name/Alias:	Formula:
STYRENE	STYRENE	C8H8
SULFUR DIOXIDE	SO2	O2S
SULFURIC ACID	H2SO4	H2O4S
TOLUENE	TOLUENE	C7H8
TRIETHYLENE GLYCOL	TEG	C6H14O4
VINYL CHLORIDE	VCL	C2H3Cl
WATER	H2O	H2O

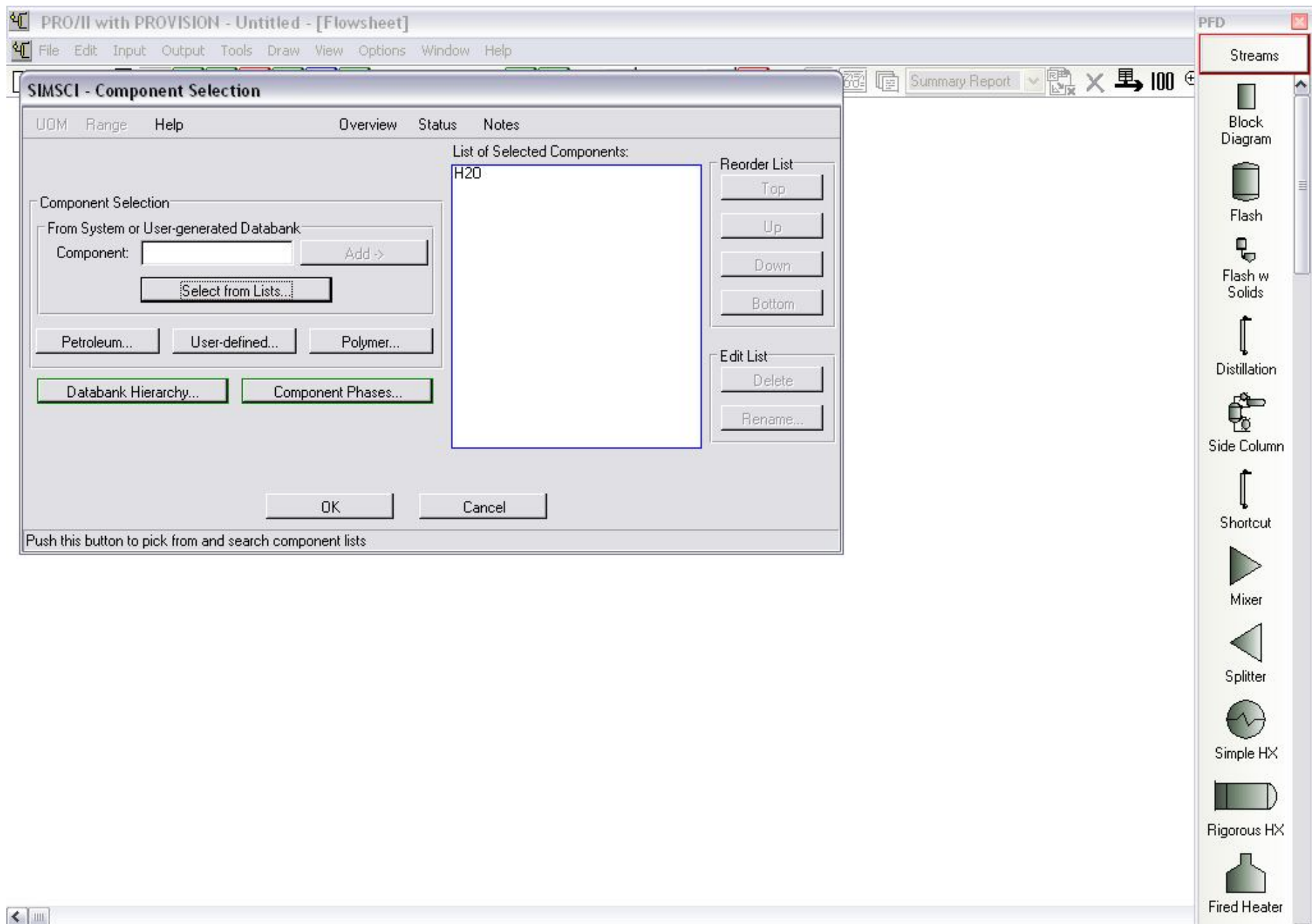
Add Components Remove Components

Additions to Component List:

WATER	H2O	H2O
-------	-----	-----

OK Cancel

Exit the window after saving all data



PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

SIMSCI - Thermodynamic Data

UDM Range Help Overview Status Notes

Selection of Property Calculation System

Category: Most Commonly Used
All Primary Methods
Equations of State
Liquid Activity
Generalized Correlations
Special Packages
Electrolyte

Primary Method:

Defined Systems:

Add ->

Default System:

Actions for Selected Property Calculation System

Modify... Delete Rename...

OK Cancel

Select an electrolyte thermodynamic system

PFD

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

Summary Report

PFD

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

SIMSCI - Thermodynamic Data

UDM Range Help Overview Status Notes

Selection of Property Calculation System

Category: Most Commonly Used All Primary Methods Equations of State Liquid Activity Generalized Correlations Special Packages Electrolyte

Primary Method: Soave-Redlich-Kwong SRK-Kabadi-Danner SRK-Huron-Vidal SRK-Panag.-Reid SRK-Modified Panag.-Reid **SRK-SIMSCI** SRK-Hexamer

Defined Systems:

Default System:

Actions for Selected Property Calculation System

Modify... Delete Rename...

OK Cancel

Add selection to list of defined property calculation systems

PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

1.2.8. Summary Report X 100

SIMSCI - Thermodynamic Data

Thermodynamic Data - Liquid-Liquid Options

UDM Range Help

The selected thermodynamic system, SRK-SIMSCI, is capable of calculating two liquid phases. By default, however, this method will only consider a single liquid phase. Choose an option below or push "OK" to accept the default.

VLE/VLE Options

☐ Single Liquid Phase Only

☒ Enable Two-Liquid-Phase Calculations

You may alter this option by changing the K-Value (LLE) selection on the window beneath the "Modify" button.

OK Cancel

Perform rigorous liquid-liquid equilibrium calculations

Defined Systems:

Add ->

Default System:

Rename...

PFD

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

SIMSCI - Thermodynamic Data

UDM Range Help Overview Status Notes

Selection of Property Calculation System

Category: Primary Method: Defined Systems:

Most Commonly Used
All Primary Methods
Equations of State
Liquid Activity
Generalized Correlations
Special Packages
Electrolyte

Soave-Redlich-Kwong
SRK-Kabadi-Danner
SRK-Huron-Vidal
SRK-Panag.-Reid
SRK-Modified Panag.-Reid
SRK-SIMSCI
SRK-Hexamer

Add ->

SRKS01

Default System:
SRKS01

Actions for Selected Property Calculation System

Modify... Delete Rename...

OK Cancel

Select a thermodynamic property calculation system

PFD

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

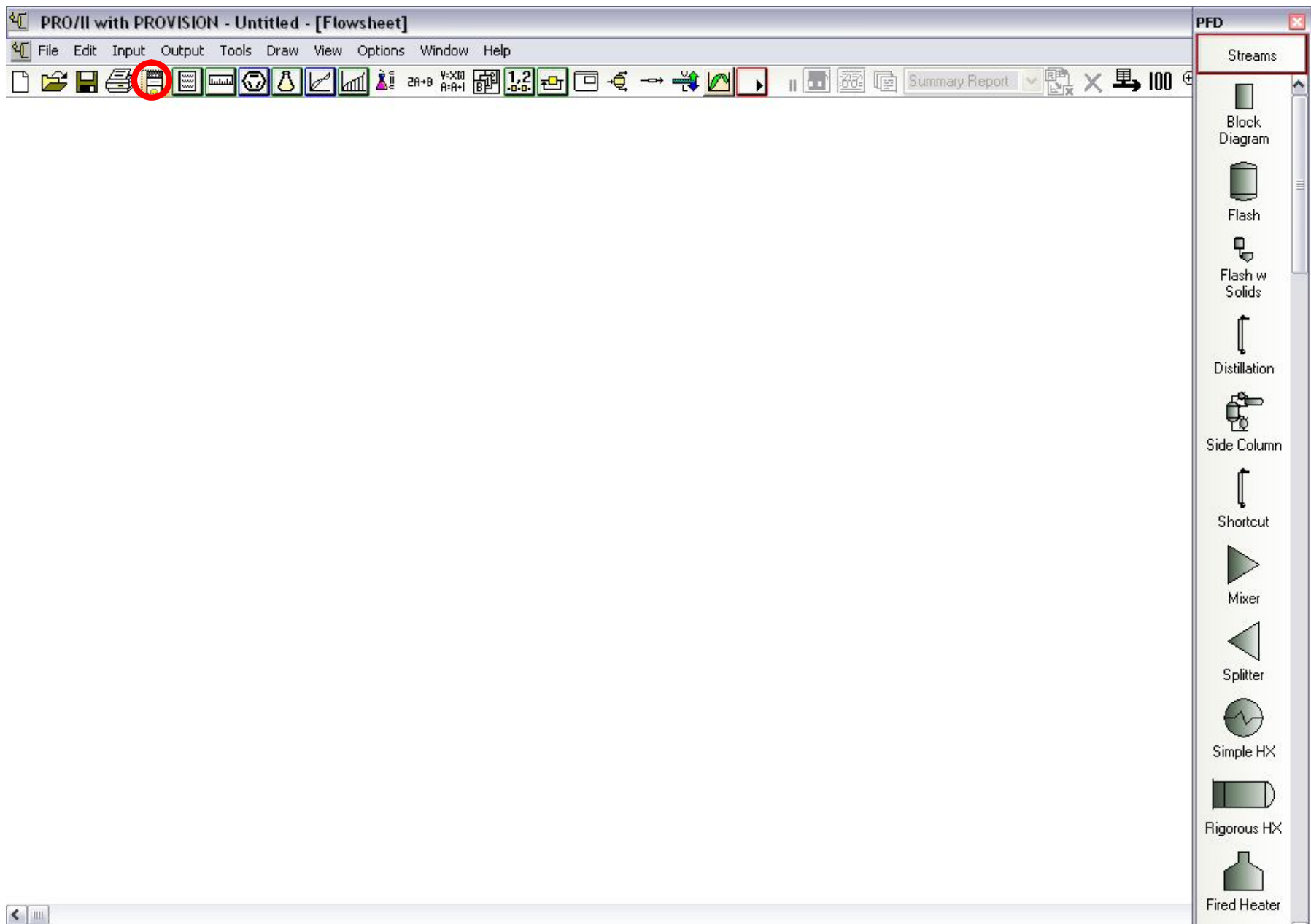
Mixer

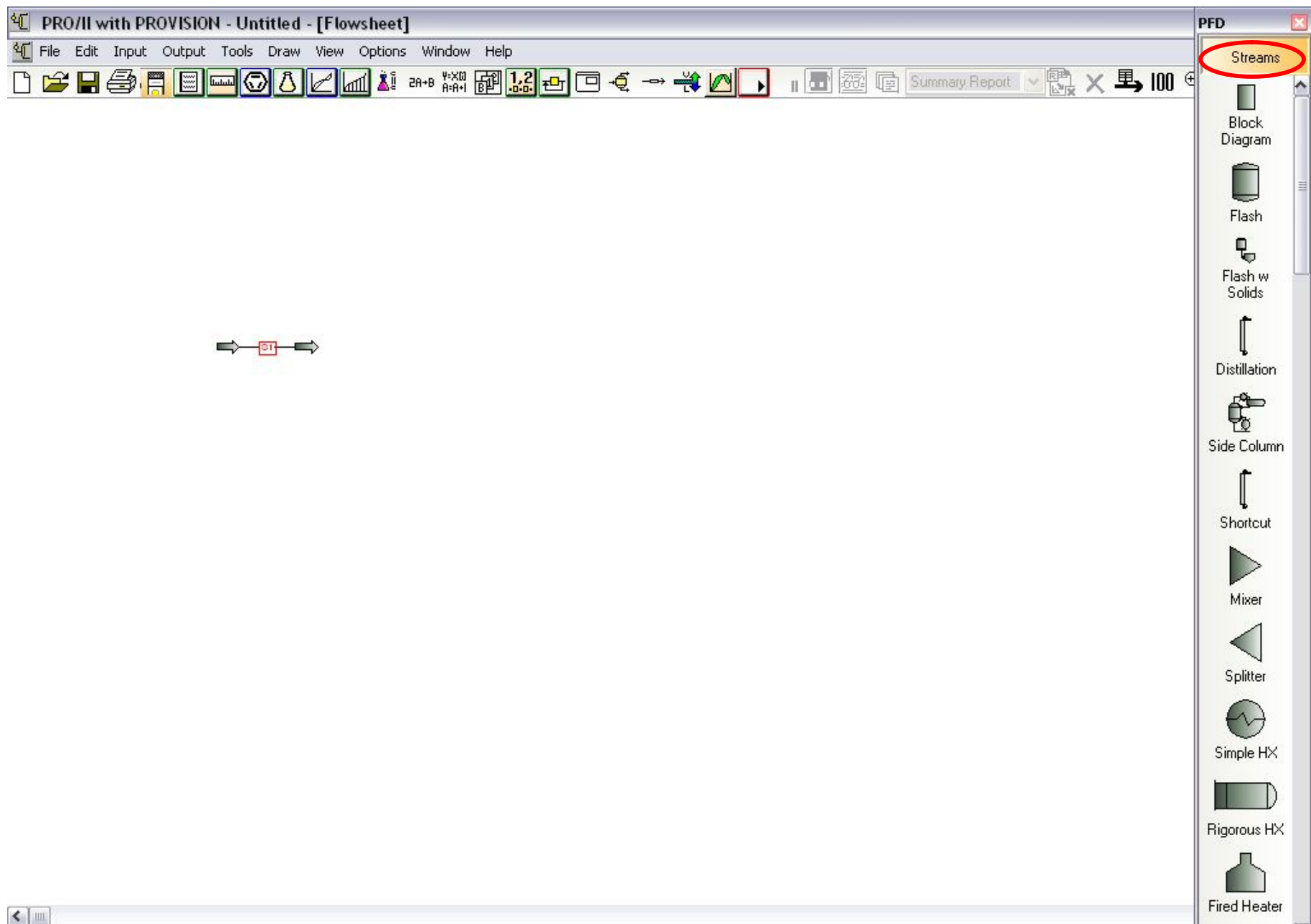
Splitter

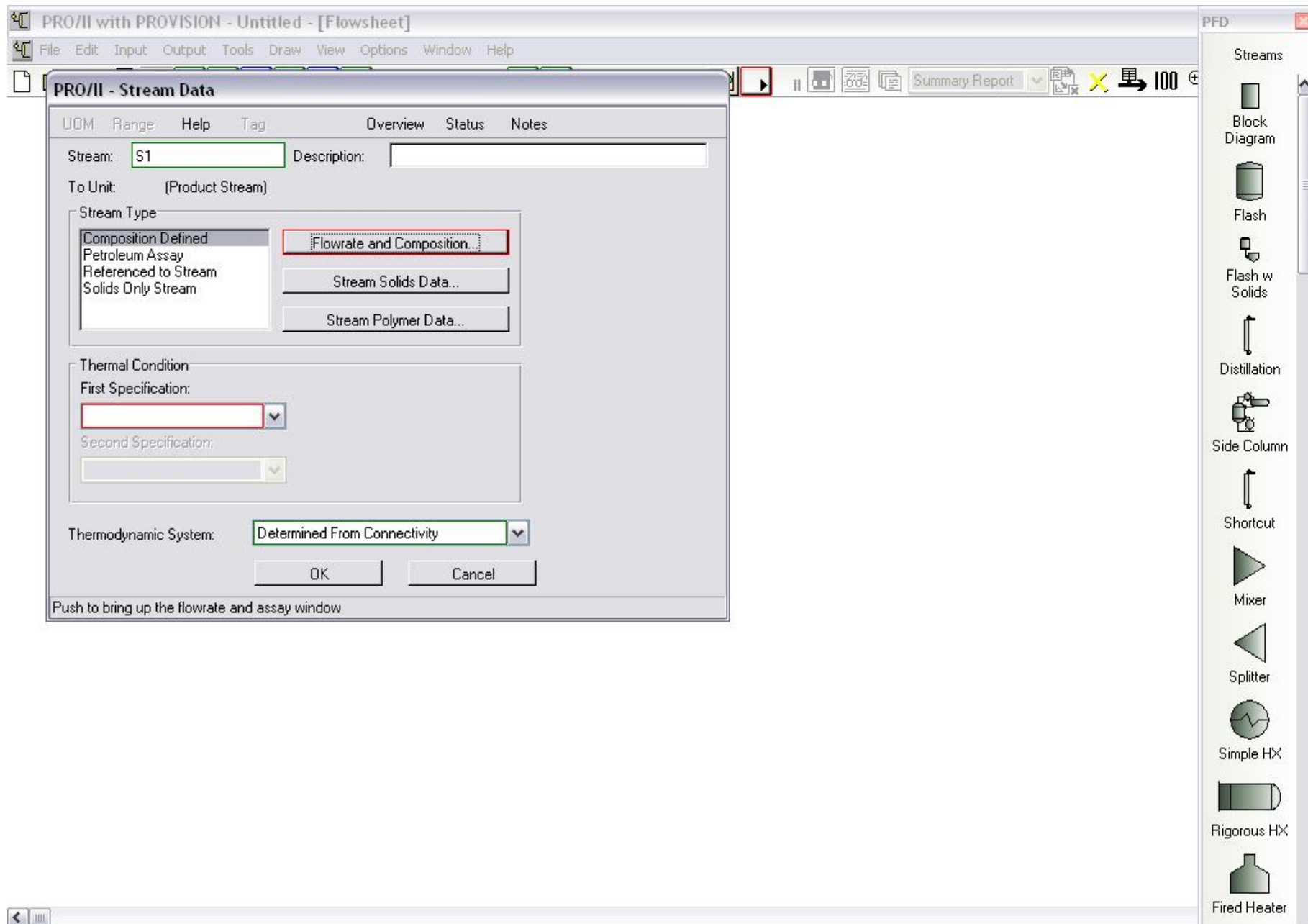
Simple HX

Rigorous HX

Fired Heater







PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

Summary Report

100

PRO/II - Stream Data

UDM Range Help Tag Overview Status Notes

Stream: S1 Description:

To Unit: (Product Stream)

Stream Type

- Composition Defined
- Petroleum Assay
- Referenced to Stream
- Solids Only Stream

Flowrate and Assay...

Stream Solids Data...

Stream Polymer Data...

Thermal Condition

First Specification:

Second Specification:

Thermodynamic System: Determined From Connectivity

OK Cancel

Select a method to define the stream

PFD

Streams

- Block Diagram
- Flash
- Flash w Solids
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- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

Summary Report

100

Stream Data - Flowrate and Assay

UOM Range Help Tag

Specify fluid flowrate and assay for stream S1

Fluid Flowrate: lb/hr

Define/Edit Assay...

This stream's composition will be divided into pseudocomponents with boiling points based on the default set of TBP cutpoints. This stream will be included in the assay blending when the properties of these pseudocomponents are generated.

OK Cancel

Enter the fluid flowrate

Thermodynamic System:

Determined From Connectivity

OK Cancel

Push to bring up the flowrate and assay window

PFD

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

Streams

- Block Diagram
- Flash
- Flash w Solids
- Distillation
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- Fired Heater

Stream Data - Flowrate and Assay

UOM Range Help Tag

Specify fluid flowrate and assay for stream S1

Convert Units-of-Measure

Change lb/hr to bbl/day.

☐ Long descriptions

Basis:

Mass		
Liq. Vol.	ft3	sec
	gal	min
	bbl	hr
	cm3	day
	liter	wk
	m3	mon
	mm3	yr

Change Units Convert Value Cancel

Thermodynamic System: Determined From Connectivity

OK Cancel

Push to bring up the flowrate and assay window

PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

Summary Report

100

Stream Data - Flowrate and Assay

UOM Range Help Tag

Specify fluid flowrate and assay for stream S1

Fluid Flowrate: bbl/day

Define/Edit Assay...

This stream's composition will be divided into pseudocomponents with boiling points based on the **default set of TBP cutpoints**. This stream will be **included in** the assay blending when the properties of these pseudocomponents are generated.

OK Cancel

Enter the fluid flowrate

Thermodynamic System:

OK Cancel

Push to bring up the flowrate and assay window

PFD

Streams

- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

Stream Data - Assay Definition

UOM Range Help Tag

Assay data for stream S1

Distillation

- ☐ True Boiling Point
- ☐ ASTM D86
- ☒ ASTM D1160
- ☐ ASTM D2887

Pressure: 14.696 psia

☐ Correct for Cracking
(Recommended for API 63 and
Edmister-Okamoto Interconversion only)

Gravity Data

- ☐ API Gravity
- ☐ Specific Gravity
- ☐ Watson K-Factor

Average:

Gravity Curve:

Additional Data

Molecular Weight... Refinery Inspection Properties...
Lightends... User-defined Special Properties...

OK Cancel

Exit the window after saving all data

Streams

- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

	Cut	Percent Distilled	Temperature F
1			
2			
3			
4			
5			
6			
7			
8			
9			
10			

View Curve...

PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

Stream Data - Assay Definition

UOM Range Help Tag

Assay data for stream S1

Distillation

- ☒ True Boiling Point
- ☐ ASTM D86
- ☐ ASTM D1160
- ☐ ASTM D2887

TBP Basis

- ☒ Liquid Volume
- ☐ Weight

Pressure: 14.696 psia

☐ Correct for Cracking
(Recommended for API 63 and Edmister-Okamoto Interconversion only)

Gravity Data

- ☐ API Gravity Average:
- ☐ Specific Gravity
- ☐ Watson K-Factor

Additional Data

-
-

Select TBP distillation

Cut	Percent Distilled	Temperature F
Copy		
Paste		
Insert		
1		
2		
3		
4		
5		
6		
7		
8		
9		
10		

Streams

- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

Stream Data - Assay Definition

UOM Range Help Tag

Assay data for stream S1

Distillation

- ☒ True Boiling Point
- ☐ ASTM D86
- ☐ ASTM D1160
- ☐ ASTM D2887

TBP Basis

- ☒ Liquid Volume
- ☐ Weight

Pressure: 14.696 psia

☐ Correct for Cracking
(Recommended for API 63 and Edmister-Okamoto Interconversion only)

Gravity Data

- ☒ API Gravity Average: 8.99
- ☐ Specific Gravity
- ☐ Watson K-Factor

Gravity Curve...

Additional Data

- Molecular Weight...
- Refinery Inspection Properties...
- Lightends...
- User-defined Special Properties...

OK Cancel

Enter the average gravity

Cut	Percent Distilled	Temperature F
1	0.00	379.20
2	1.00	440.39
3	2.00	497.09
4	3.50	550.72
5	5.00	588.64
6	7.50	642.16
7	10.00	658.17
8	12.50	682.46
9	15.00	699.58
10	17.50	727.99

View Curve...

Streams

- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
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- Fired Heater

PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Stream Data

UGM Range Help Tag Overview Status Notes

Stream: S1 Description:

To Unit: (Product Stream)

Stream Type

- Composition Defined
- Petroleum Assay
- Referenced to Stream
- Solids Only Stream

Flowrate and Assay...

Stream Solids Data...

Stream Polymer Data...

Thermal Condition

First Specification:

Second Specification:

Thermodynamic System: Determined From Connectivity

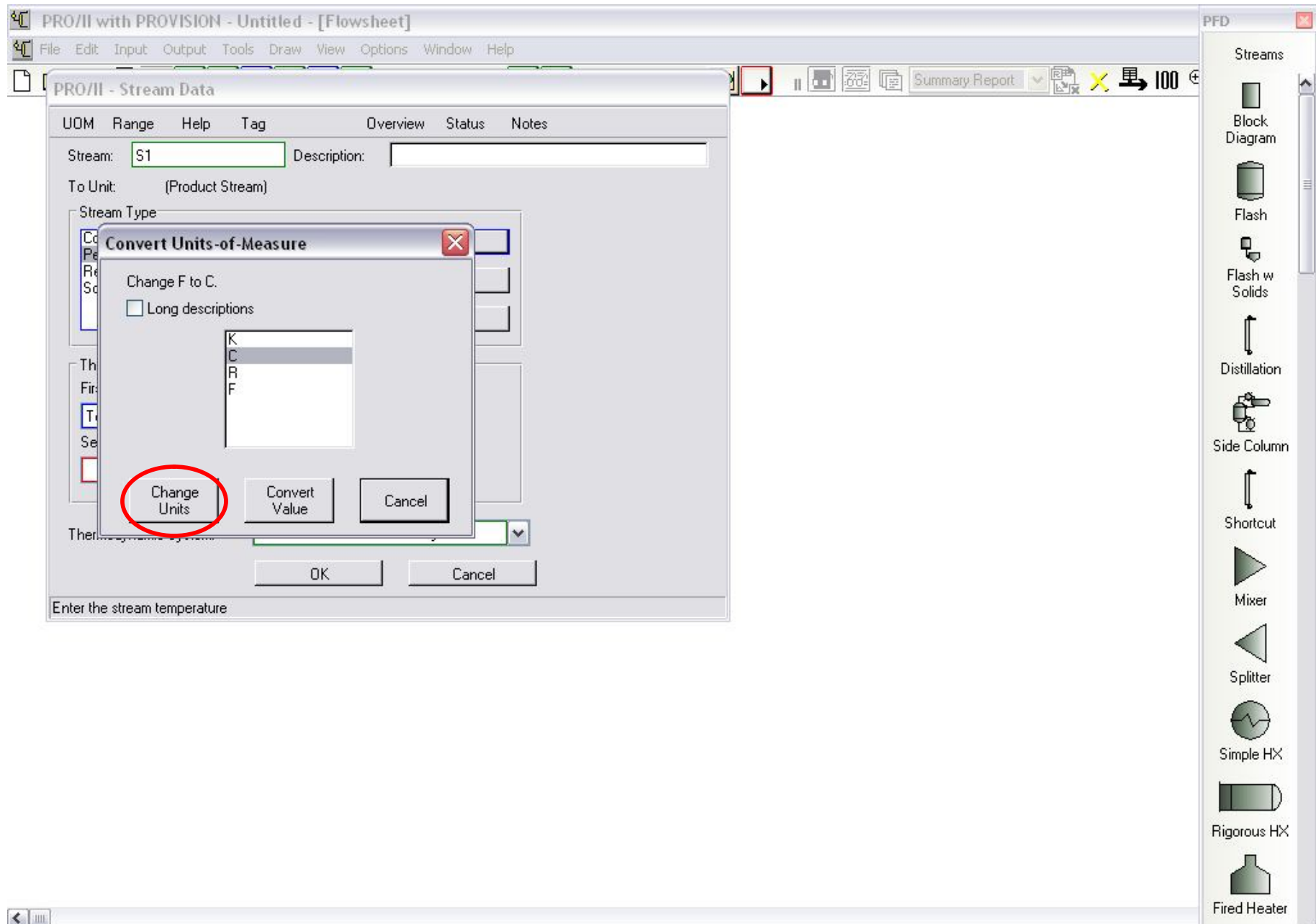
OK Cancel

Push to bring up the flowrate and assay window

PFD

Streams

- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater



PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Stream Data

UOM Range Help Tag Overview Status Notes

Stream: S1 Description:

To Unit: (Product Stream)

Stream Type

Convert Units-of-Measure

Change psia to psig.

☐ Long descriptions

psia
psig
atm
kPa
kPag
kg/cm2
kg/cm2a

Change Units Convert Value Cancel

OK Cancel

Enter stream pressure

PFD

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

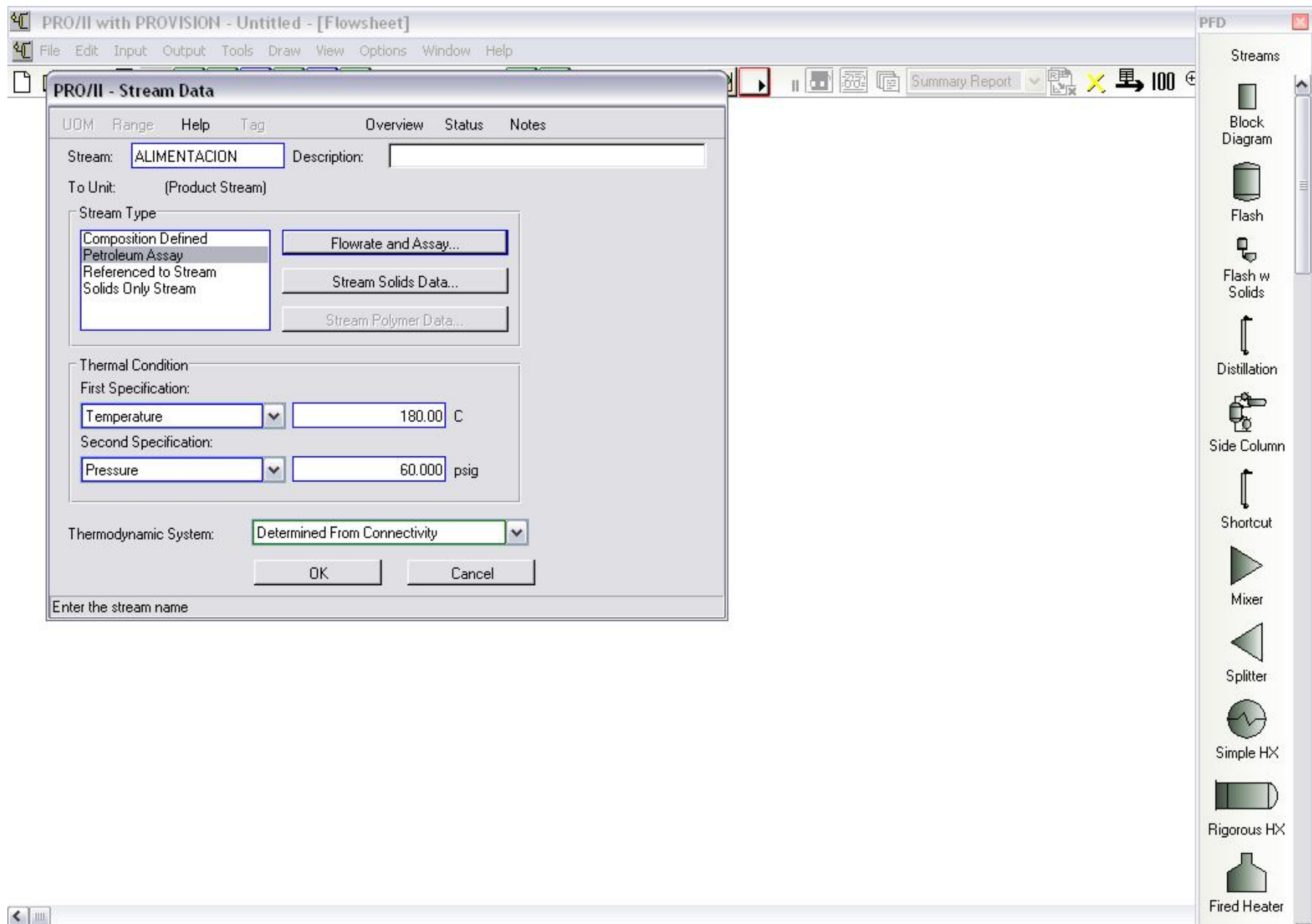
Mixer

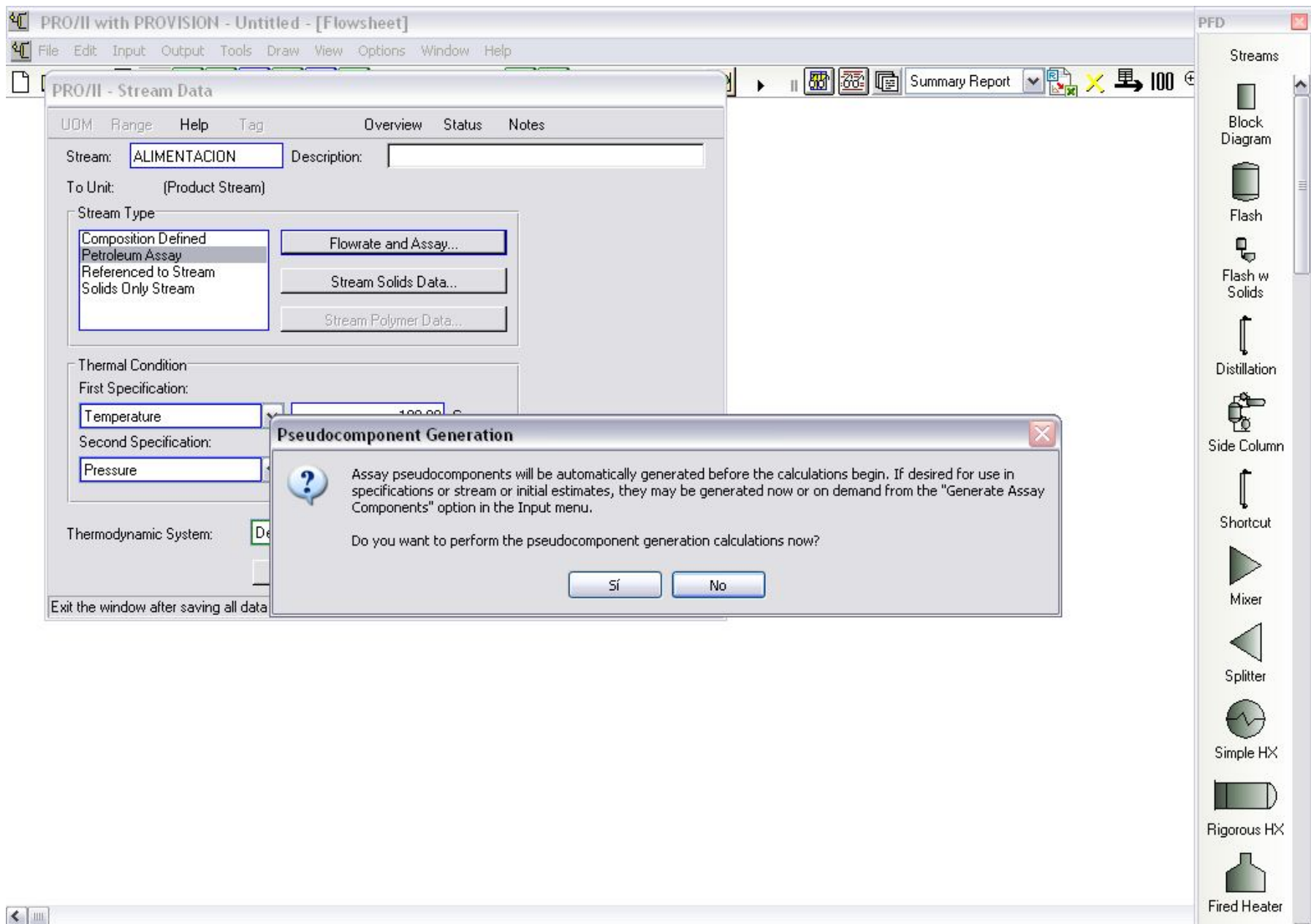
Splitter

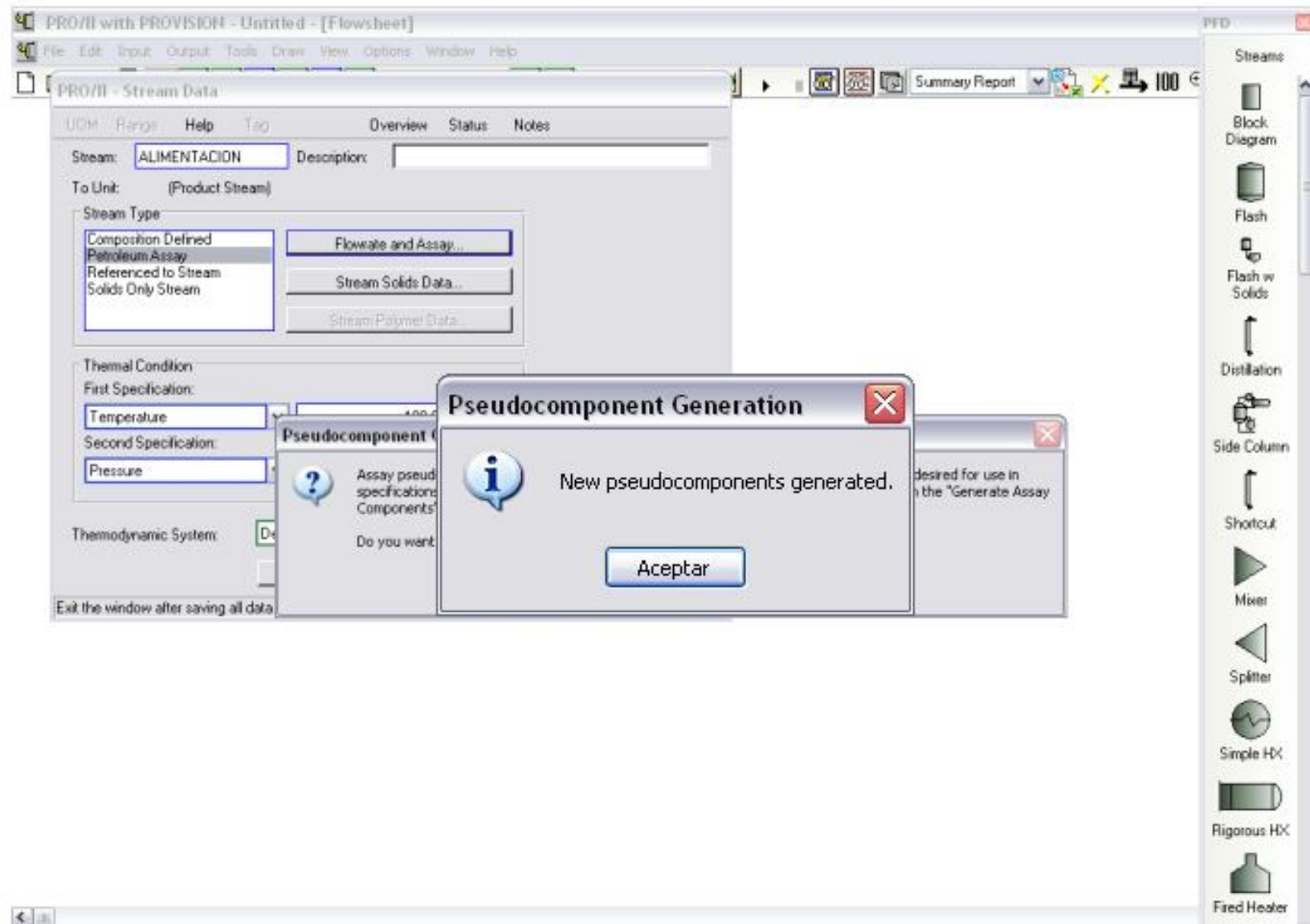
Simple HX

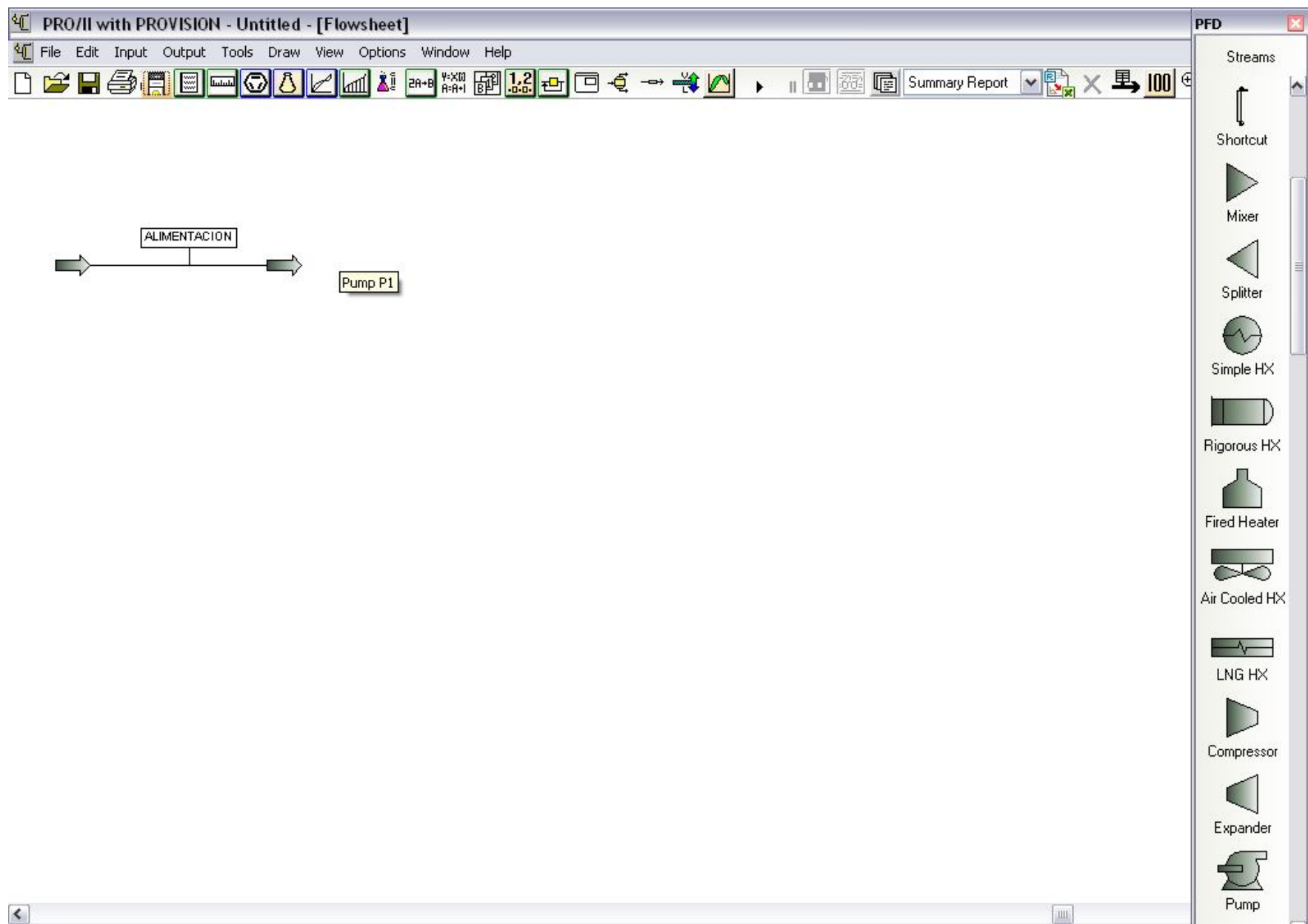
Rigorous HX

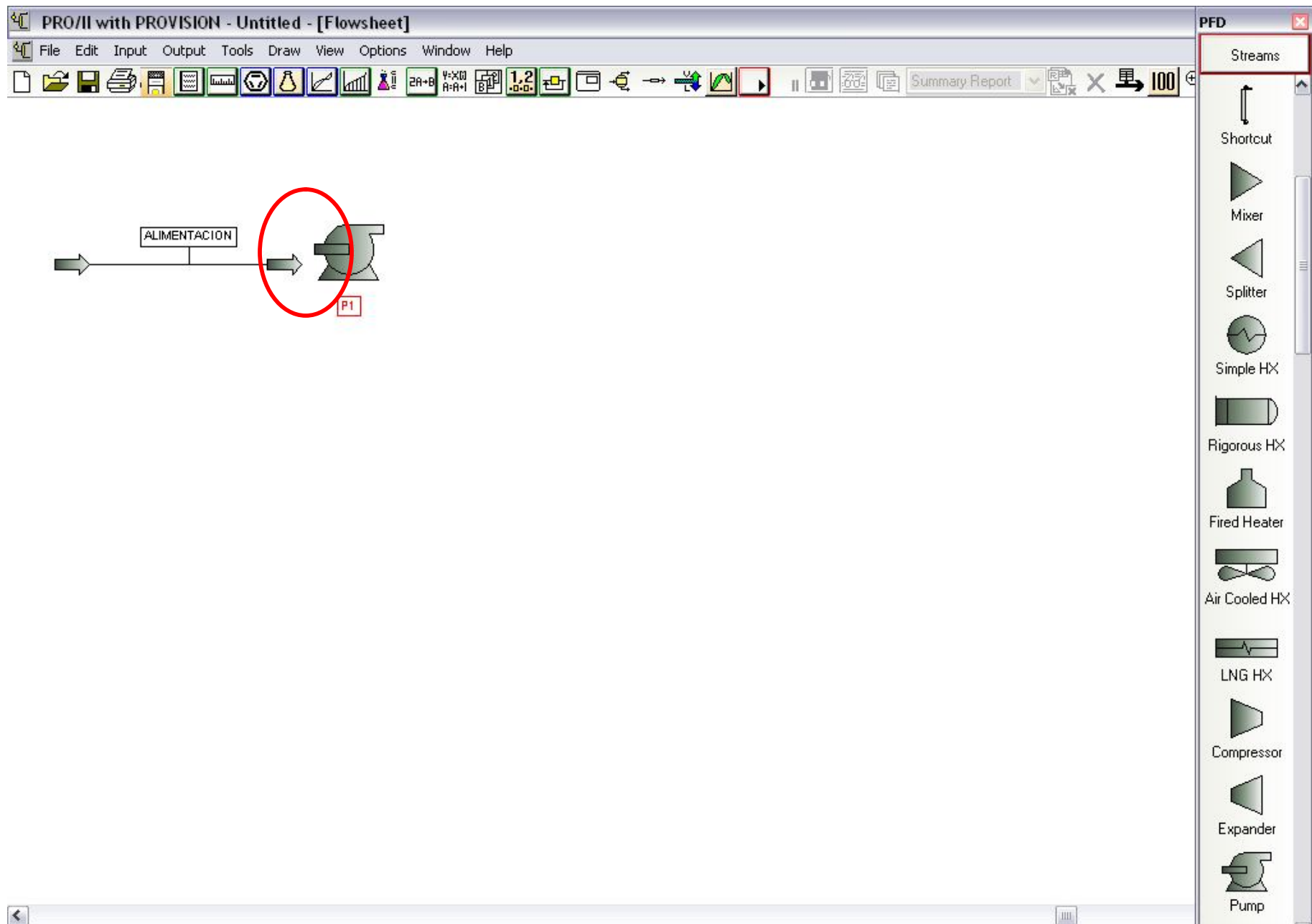
Fired Heater

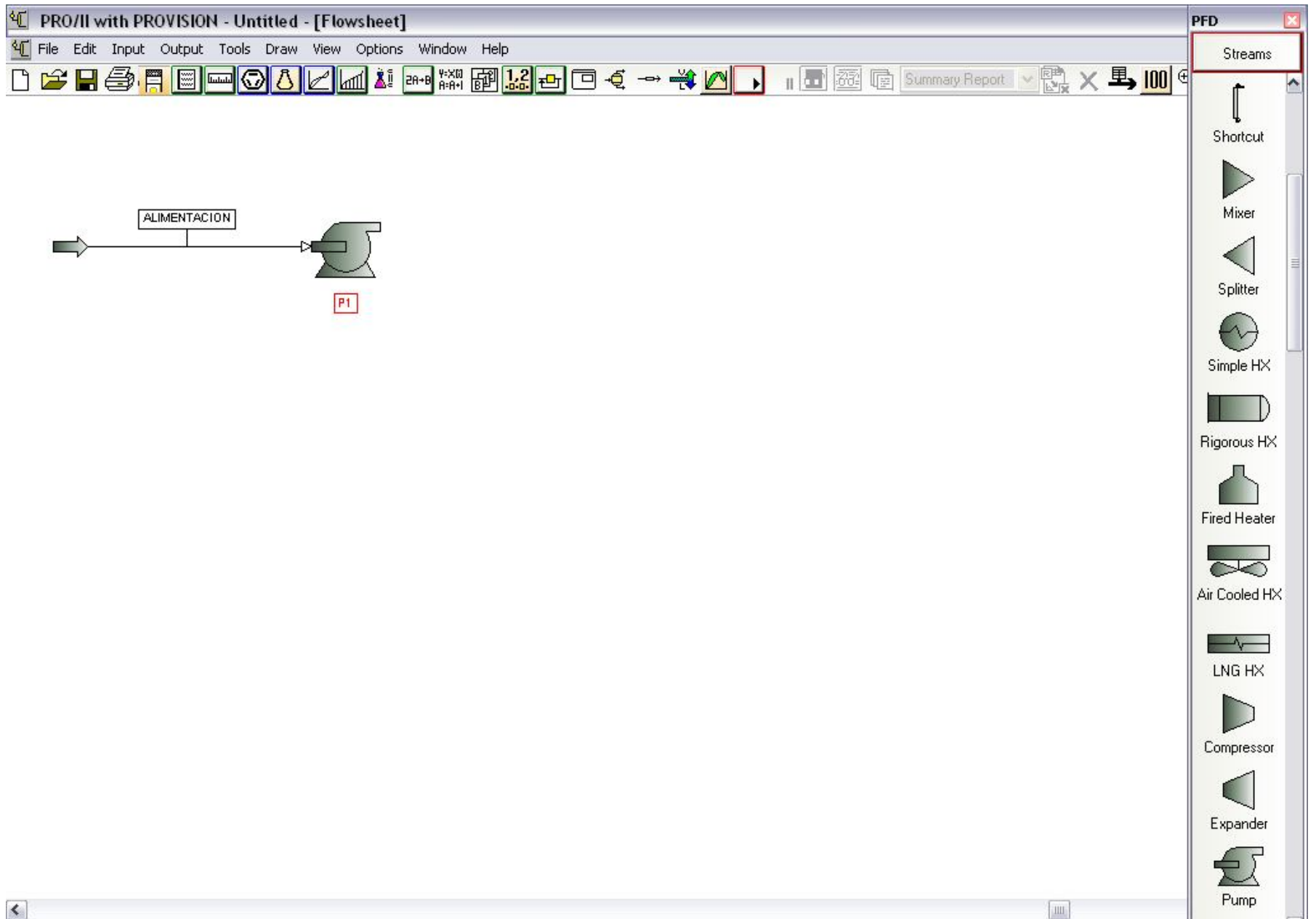


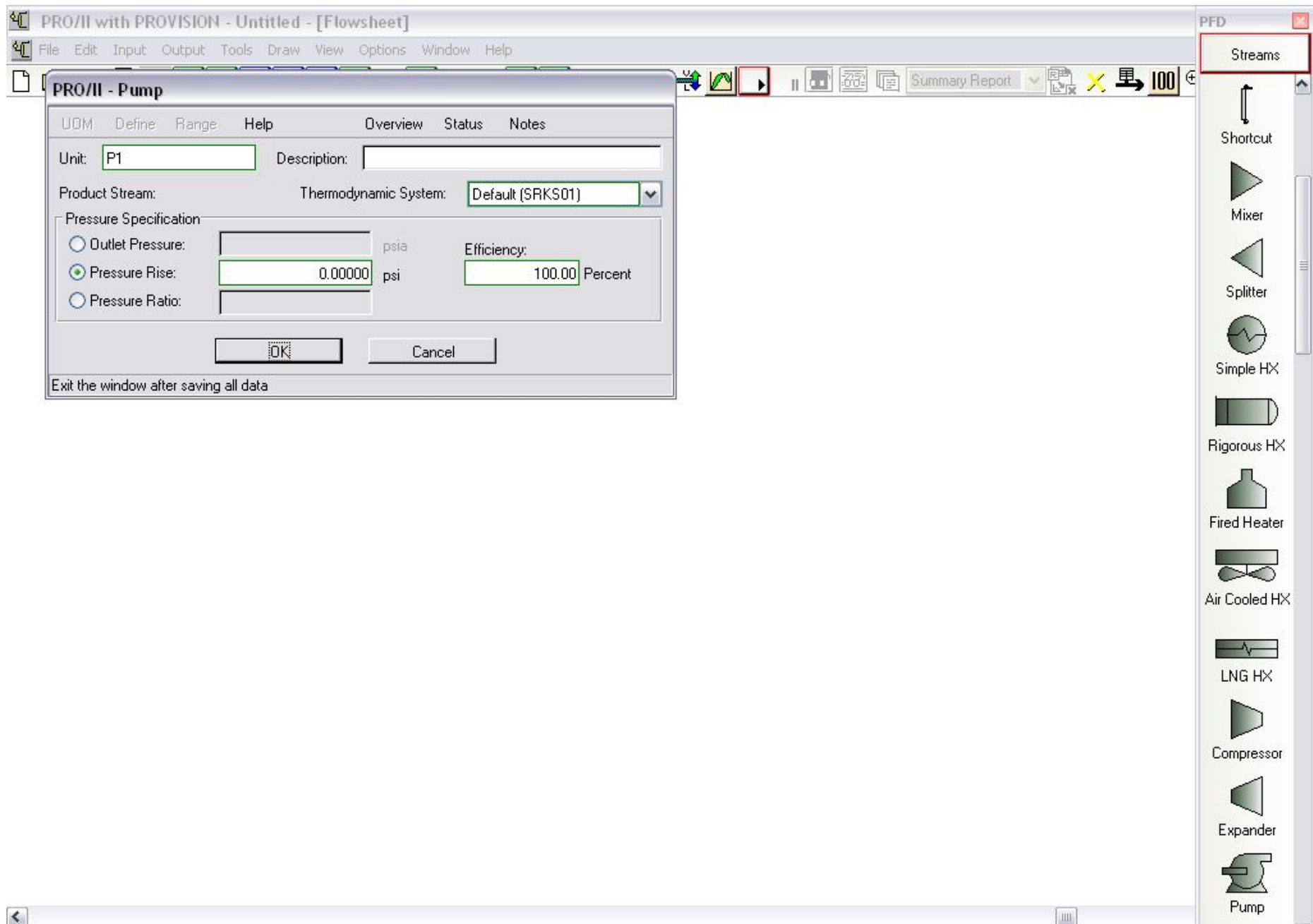












PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Pump

UQM Define Range Help Overview Status Notes

Unit: P1 Description:

Product Stream: Thermodynamic System: Default (SRKS01)

Pressure Specification

☒ Outlet Pressure: psia Efficiency: 80.00 Percent

☐ Pressure Rise: 0.00000 psi

☐ Pressure Ratio:

OK Cancel

Enter the outlet pressure value

Convert Units-of-Measure

Change psia to psig.

☐ Long descriptions

psia
psig
atm
kPa
kPag
kg/cm2
kq/cm2q

Change Units Convert Value Cancel

PFD

Streams

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

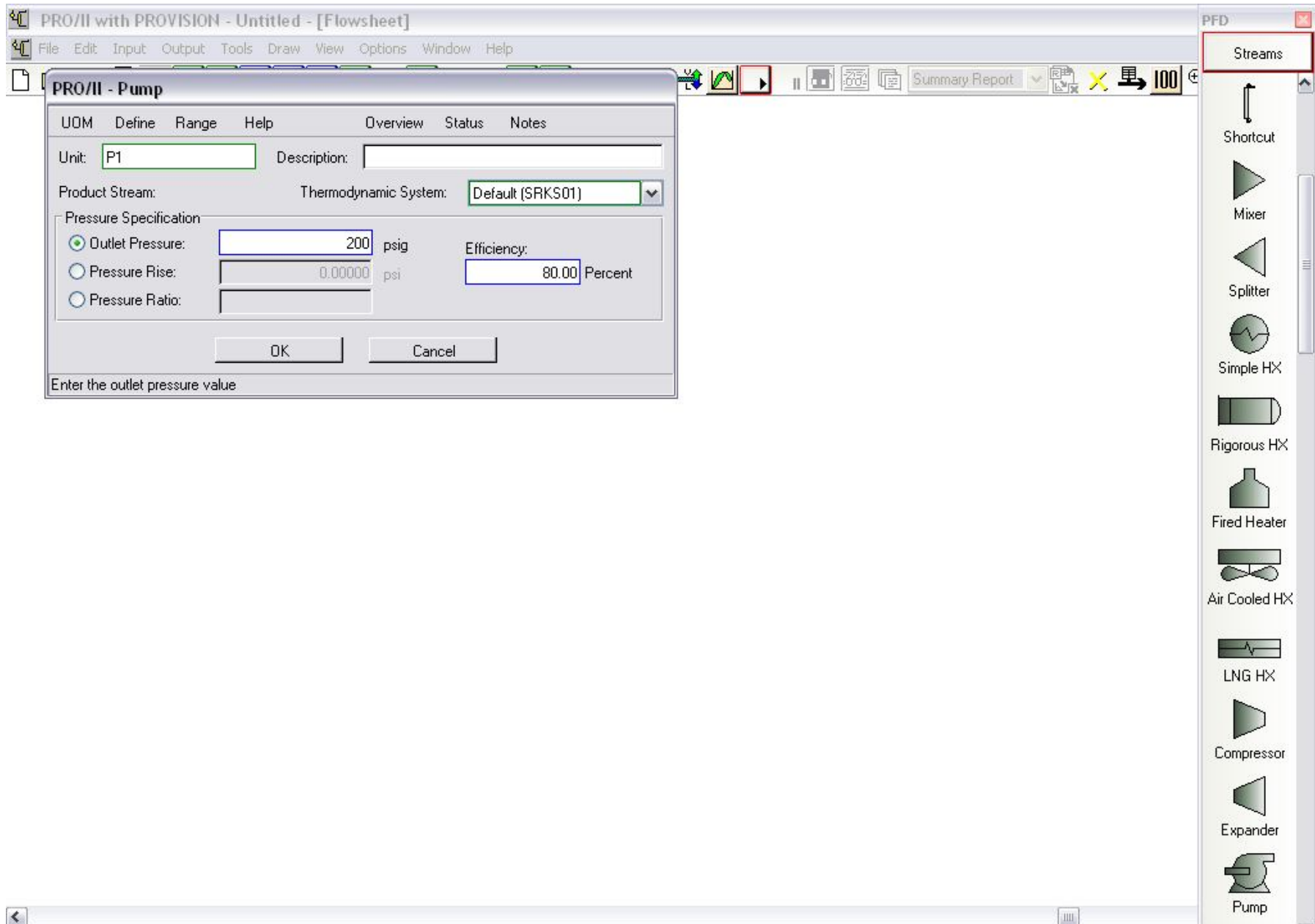
Air Cooled HX

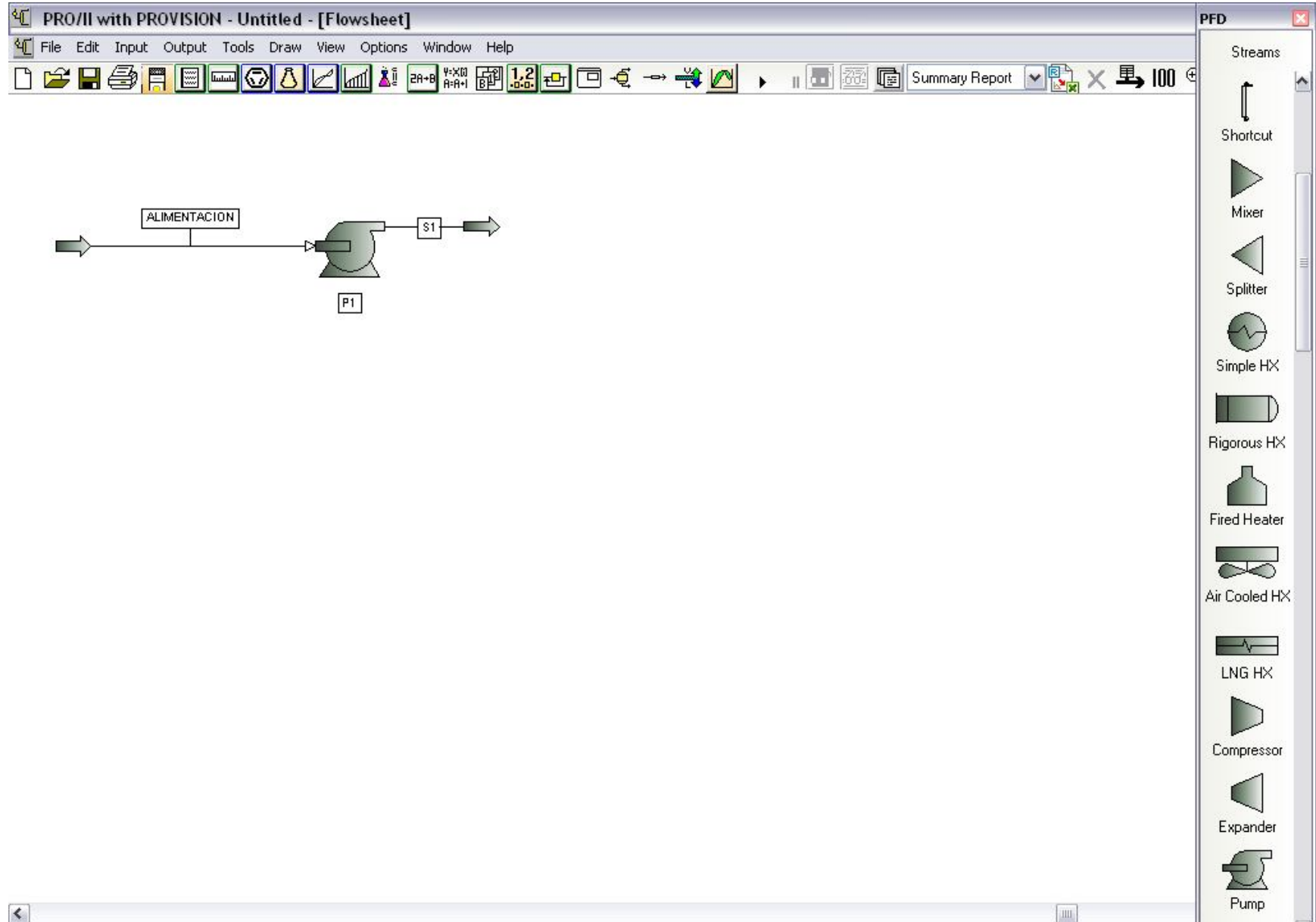
LNG HX

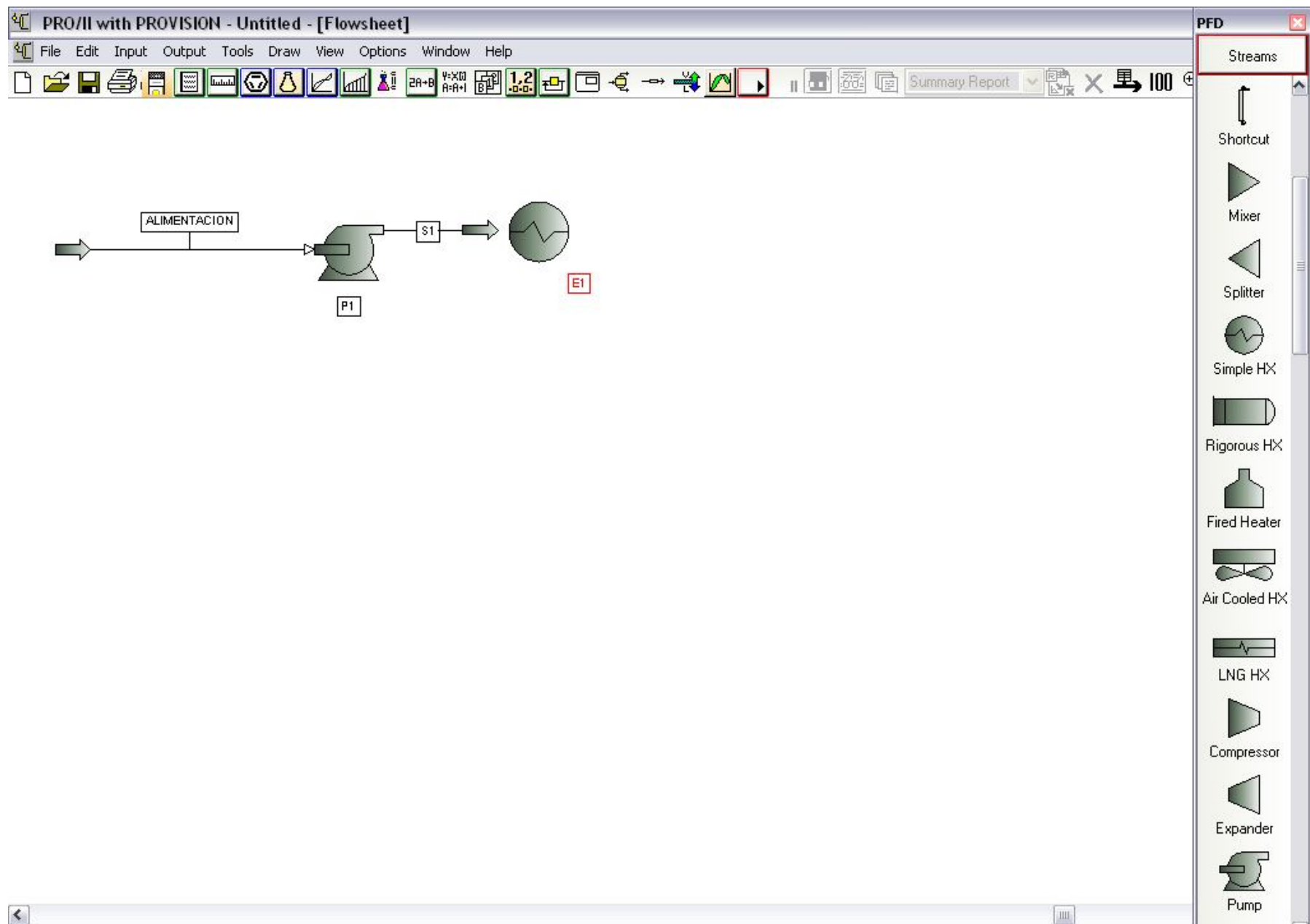
Compressor

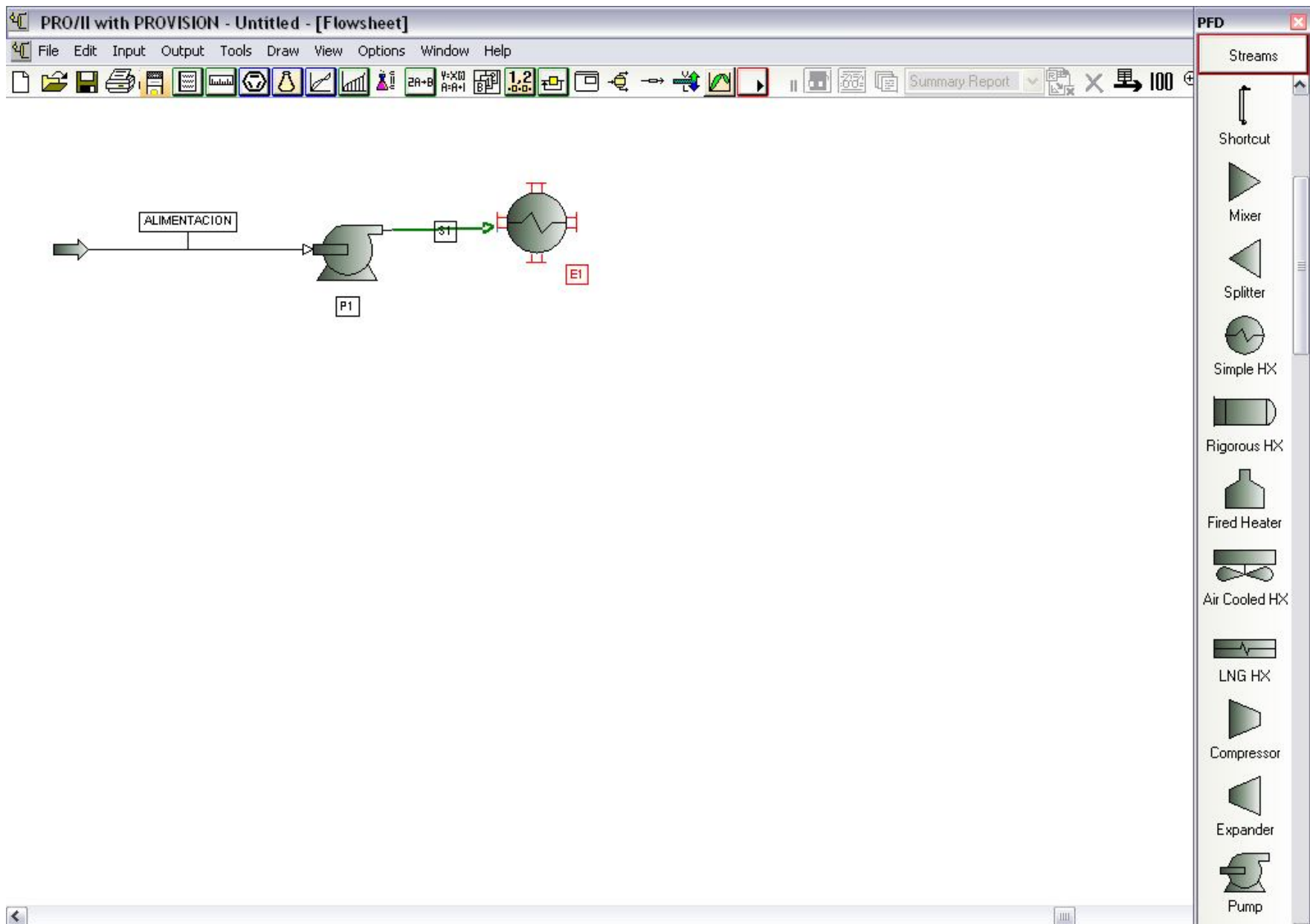
Expander

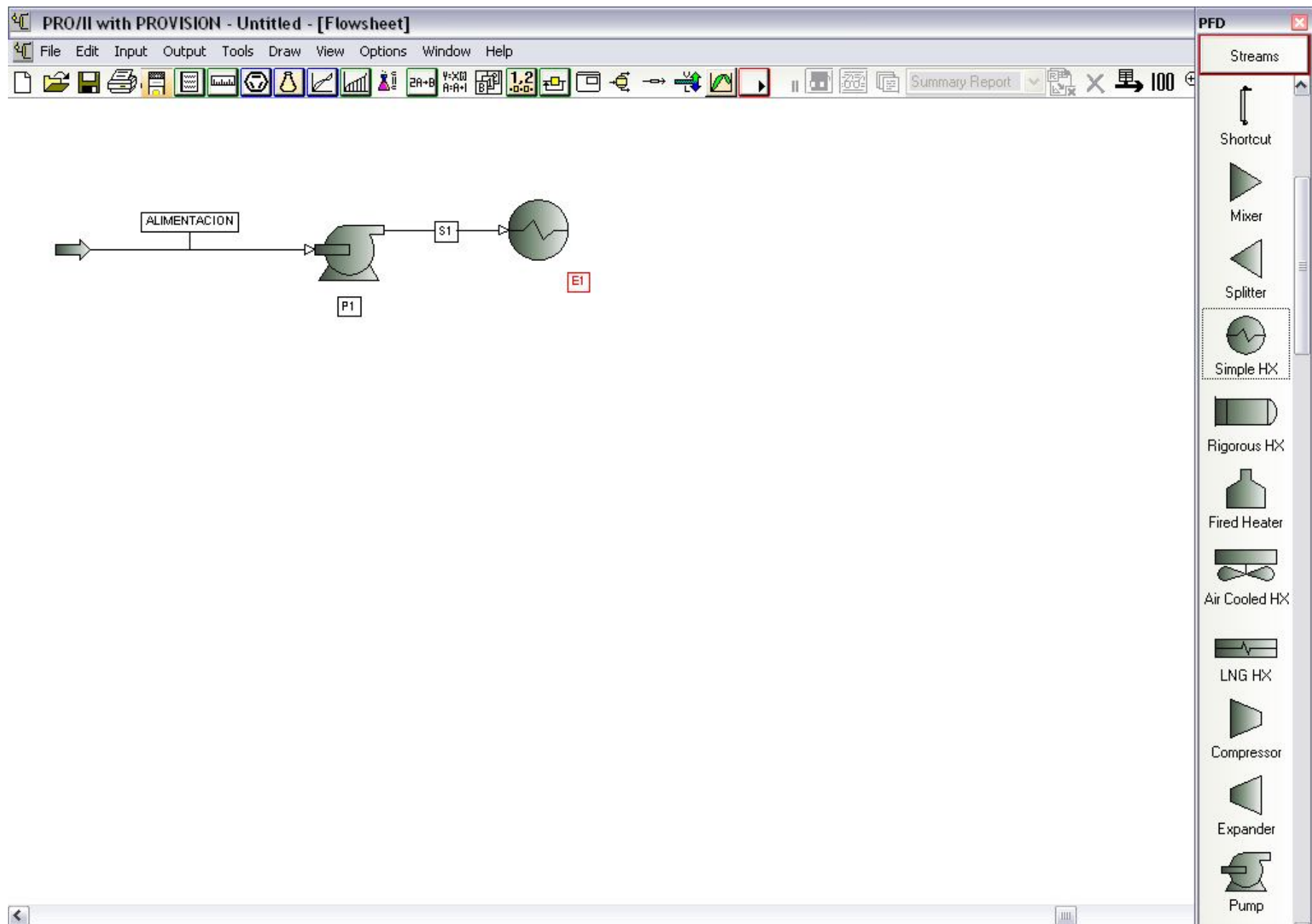
Pump











PRO/II with PROVISION - Untitled - [Flowsheet]

File Edit Input Output Tools Draw View Options Window Help

Summary Report

100

PRO/II - Heat Exchanger

UOM Define Range Help Overview Status Notes

Unit: E1 Description:

Hot Side

Process Stream...
Utility Stream...
Attach to Column...

Pressure Drop: 0.00000 psi

Thermodynamic System: Default (SRKS01)

Cold Side

Process Stream...
Utility Stream...
Attach to Column...

Pressure Drop: 0.00000 psi

Thermodynamic System: Default (SRKS01)

Specification...
Configuration...
Zones Analysis...
Print Options...

OK
Cancel

Push to bring up the process stream window

PFD

Streams

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

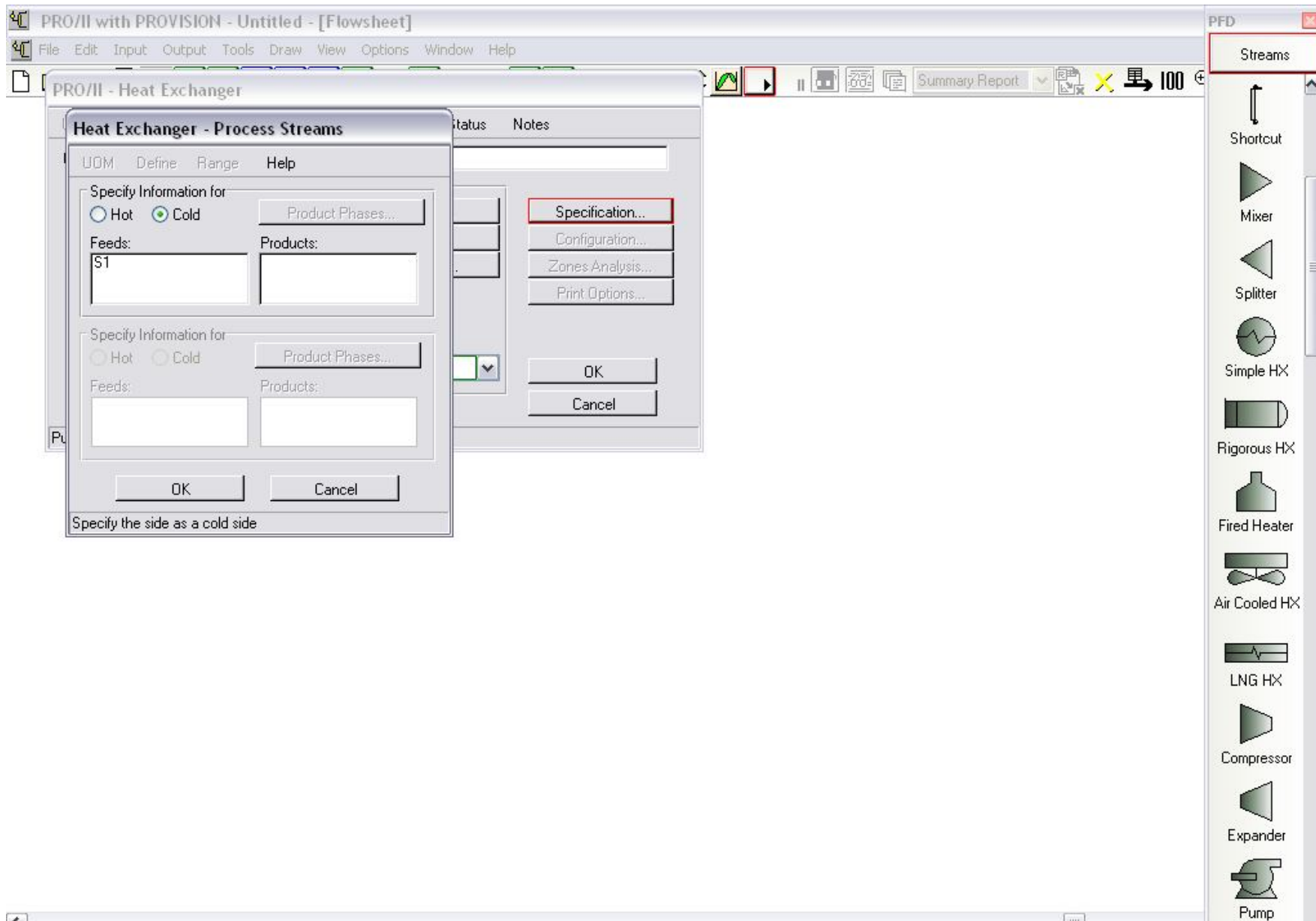
Air Cooled HX

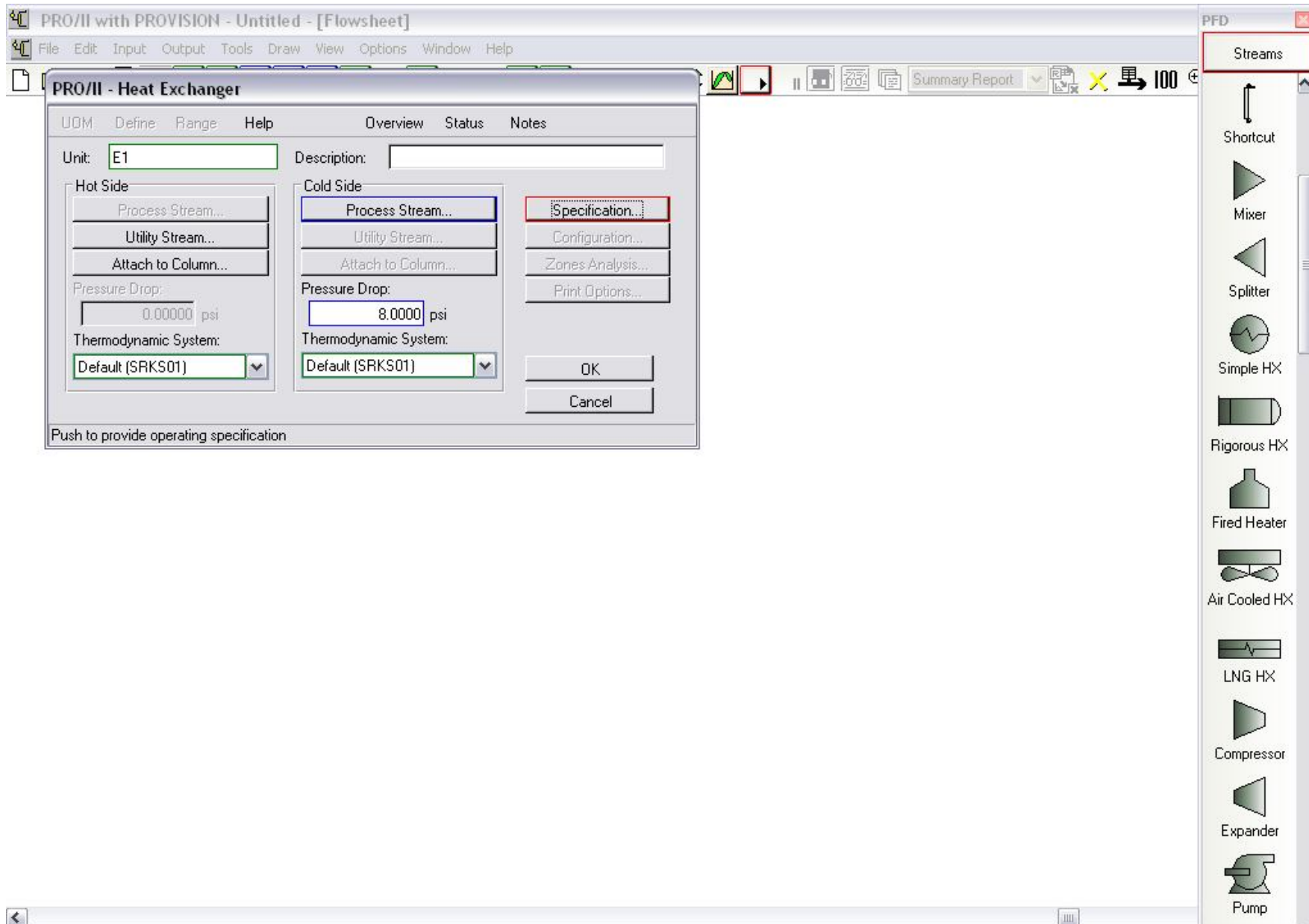
LNG HX

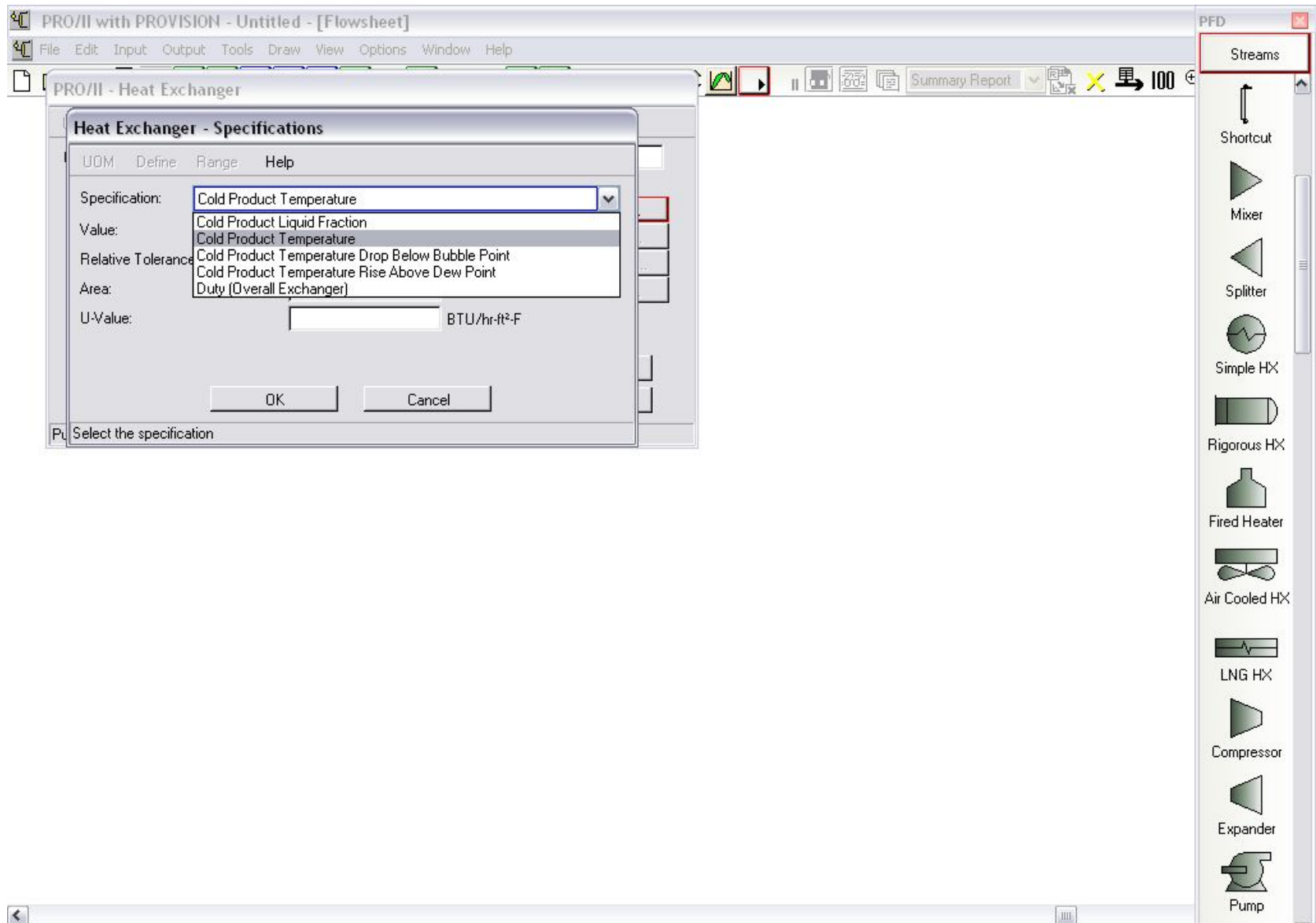
Compressor

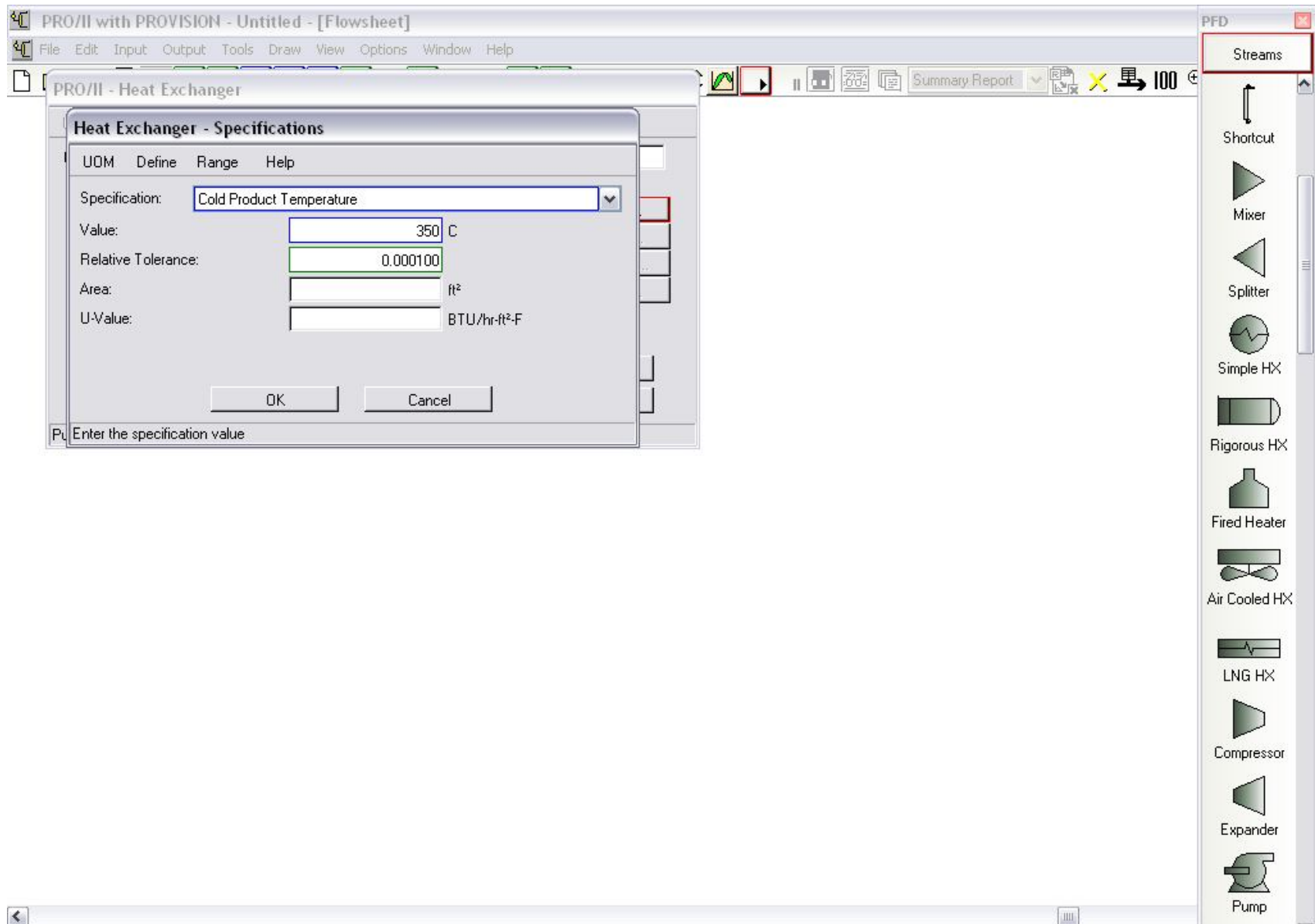
Expander

Pump









PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

Flowsheet

```
graph LR; Alimentacion[ALIMENTACION] --> P1[P1]; P1 -- S1 --> E1((E1)); E1 -- S2 --> Exit[ ];
```

caso base uc Solved

*** THIS RUN USED 10.48 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:07:13	01/07/09	NO ERRORS
FINISHED	15:07:15	01/07/09	NO WARNINGS
RUN TIMES			NO MESSAGES
INTERACTIVE	0 MIN,	0.00 SEC	
CALCULATIONS	0 MIN,	1.79 SEC	
TOTAL	0 MIN,	1.79 SEC	

PFD

- Streams
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater
- Air Cooled HX
- LNG HX
- Compressor
- Expander
- Pump

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

Flowsheet

ALIMENTACION

S1

S2

Data Review Window

View Results

View Excel Results

Data Entry...

Notes...

Copy

Goto

Break Before

Break After

Collapse

Exclude Unit

Delete

Rotate

Flip

Restore Icon Size

Restore Label Position

Center in View

Lock

Unlock

Display...

Rename...

Add to Active Report

Solving caso base uc

*** THIS RUN USED 10.48 PRO/II S

*** RUN STATISTICS

STARTED 15:07:13 01/07/09

FINISHED 15:07:15 01/07/09

RUN TIMES

INTERACTIVE 0 MIN, 0.0

CALCULATIONS 0 MIN, 1.7

TOTAL 0 MIN, 1.7

Streams

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

Air Cooled HX

LNG HX

Compressor

Expander

Pump

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

Programmer's File Editor

File Edit Options Template Execute Macro Window Help

Documents and Settings\miajaa\Configuración local\Temp\VW155.tmp

Pump 'P1'

Feeds ALIMENTACION
Products S1

	User Input	Calculated
Temperature, F		356.25
Pressure, PSIA	214.70	214.70
Pressure Rise, PSI		140.00
Work, HP		78.80
Head, FT		354.16
Efficiency	80.00	80.00

Ln 1 Col 1 15 WR Rec Off No Wrap DOS INS NUM

*** RUN STATISTICS
STARTED 15:07:13 01/07/09 NO ERRORS
FINISHED 15:07:15 01/07/09 NO WARNINGS
RUN TIMES NO MESSAGES
INTERACTIVE 0 MIN, 0.00 SEC
CALCULATIONS 0 MIN, 1.79 SEC
TOTAL 0 MIN, 1.79 SEC

PFD

Streams

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

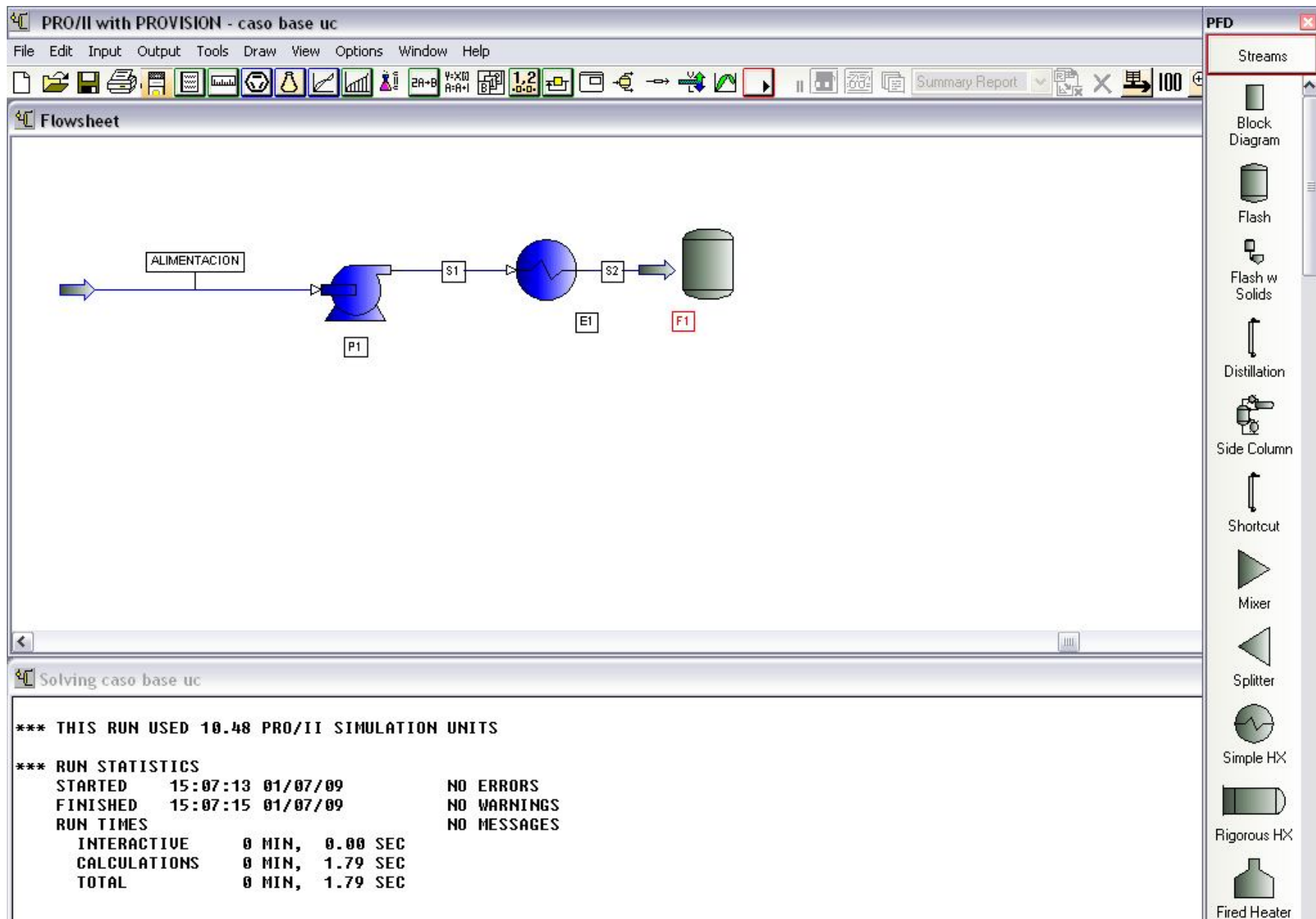
Air Cooled HX

LNG HX

Compressor

Expander

Pump



PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

Flowsheet

```
graph LR; Inlet[ALIMENTACION] --> P1[P1]; P1 -- S1 --> E1((E1)); E1 -- S2 --> F1[F1];
```

Streams

- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

Solving caso base uc

*** THIS RUN USED 10.48 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:07:13	01/07/09	NO ERRORS
FINISHED	15:07:15	01/07/09	NO WARNINGS
RUN TIMES			NO MESSAGES
INTERACTIVE	0 MIN,	0.00 SEC	
CALCULATIONS	0 MIN,	1.79 SEC	
TOTAL	0 MIN,	1.79 SEC	

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

Flowsheet

```
graph LR; Alimentacion[ALIMENTACION] --> P1[P1]; P1 -- S1 --> EI[EI]; EI -- S2 --> Tank[Tank]; F1[F1] -- S3 --> Tank
```

Solving caso base uc

*** THIS RUN USED 10.48 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:07:13	01/07/09	NO ERRORS
FINISHED	15:07:15	01/07/09	NO WARNINGS
RUN TIMES			NO MESSAGES
INTERACTIVE	0 MIN,	0.00 SEC	
CALCULATIONS	0 MIN,	1.79 SEC	
TOTAL	0 MIN,	1.79 SEC	

Add new Units/Streams from PFD Palette. Double-click on Units/Streams for input.

PFD

- Streams
- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

PRO/II - Stream Data

UQM Range Help Tag Overview Status Notes

Stream: S3 Description:

To Unit: F1

Stream Type

- Composition Defined
- Petroleum Assay
- Referenced to Stream
- Solids Only Stream

Flowrate and Composition...

Stream Solids Data...

Stream Polymer Data...

Thermal Condition

First Specification:

Second Specification:

Thermodynamic System: Determined From Connectivity

OK Cancel

Push to bring up the flowrate and assay window

PFD

Streams

- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

Solving caso base uc

*** THIS RUN USED 10.48 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:07:13	01/07/09	NO ERRORS
FINISHED	15:07:15	01/07/09	NO WARNINGS
RUN TIMES			NO MESSAGES
INTERACTIVE	0 MIN,	0.00 SEC	
CALCULATIONS	0 MIN,	1.79 SEC	
TOTAL	0 MIN,	1.79 SEC	

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Stream Data

Stream Data - Flowrate and Composition

UOM Range Help Tag

Specify flowrate and composition for stream S3

Fluid Flowrate Specification

☒ Total Fluid Flowrate: lb-mol/hr

☐ Individual Component Flowrates

Copy	Component	Composition
Paste		Mole
	H2O	
	NBP 389	
	NBP 412	
	NBP 437	
	NBP 462	
	NBP 487	
	NBP 513	

Clear Compositions Total: 0.00000 ☐ Normalize Component Flowrates Based on Specified Fluid Flowrate

OK Cancel

Enter the total fluid flowrate

Convert Units-of-Measure

Change lb-mol/hr to bbl/day.

☐ Long descriptions

Basis:

Mole	ft3	sec
Mass	gal	min
Liq. Vol.	bbl	hr
Vap. Vol.	cm3	day
	liter	wk
	m3	mon
	mm3	yr

Change Units Convert Value Cancel

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

*** THIS RUN USED 10.48 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED 15:07:13 01/07/09 NO ERRORS

FINISHED 15:07:15 01/07/09 NO WARNINGS

RUN TIMES NO MESSAGES

INTERACTIVE 0 MIN, 0.00 SEC

CALCULATIONS 0 MIN, 1.79 SEC

TOTAL 0 MIN, 1.79 SEC

Add new Units/Streams from PFD Palette. Double-click on Units/Streams for input.

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Stream Data

Stream Data - Flowrate and Composition

UOM Range Help Tag

Specify flowrate and composition for stream S3

Fluid Flowrate Specification

☒ Total Fluid Flowrate: 3000.0 bbl/day

☐ Individual Component Flowrates

Copy	Component	Composition Mole
Paste	H2O	1
	NBP 389	
	NBP 412	
	NBP 437	
	NBP 462	
	NBP 487	
	NBP 513	

Clear Compositions Total: 0.00000 ☐ Normalize Component Flowrates Based on Specified Fluid Flowrate

OK Cancel

Enter the composition

Solving caso base uc

*** THIS RUN USED 10.48 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:07:13 01/07/09	NO ERRORS
FINISHED	15:07:15 01/07/09	NO WARNINGS
RUN TIMES		NO MESSAGES
INTERACTIVE	0 MIN, 0.00 SEC	
CALCULATIONS	0 MIN, 1.79 SEC	
TOTAL	0 MIN, 1.79 SEC	

PFD

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

File Edit Input Output Tools Draw View Options Window Help

UQM Range Help Tag Overview Status Notes

Stream: S3 Description:

To Unit: F1

Stream Type

Composition Defined
Petroleum Assay
Referenced to Stream
Solids Only Stream

Flowrate and Composition...
Stream Solids Data...
Stream Polymer Data...

Thermal Condition

First Specification:

Temperature F

Second Specification:

Thermodynamic System: Determined From Connectivity

OK Cancel

Enter the stream temperature

PFD

Streams

Block Diagram
Flash
Flash w Solids
Distillation
Side Column
Shortcut
Mixer
Splitter
Simple HX
Rigorous HX
Fired Heater

Solving caso base uc

```

*** THIS RUN USED 10.48 PRO/II SIMULATION UNITS

*** RUN STATISTICS
STARTED 15:07:13 01/07/09 NO ERRORS
FINISHED 15:07:15 01/07/09 NO WARNINGS
RUN TIMES
INTERACTIVE 0 MIN, 0.00 SEC
CALCULATIONS 0 MIN, 1.79 SEC
TOTAL 0 MIN, 1.79 SEC
NO MESSAGES

```

Add new Units/Streams from PFD Palette. Double-click on Units/Streams for input.

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Stream Data

UOM Range Help Tag Overview Status Notes

Stream: S3 Description:

To Unit: F1

Stream Type

- Composition Defined
- Petroleum Assay
- Referenced to Stream
- Solids Only Stream

Flowrate and Composition...

Stream Solids Data...

Stream Polymer Data...

Thermal Condition

First Specification:

Temperature 66.00 F

Second Specification:

Pressure 200.00 psig

Thermodynamic System: Determined From Connectivity

OK Cancel

Enter stream pressure

PFD

Streams

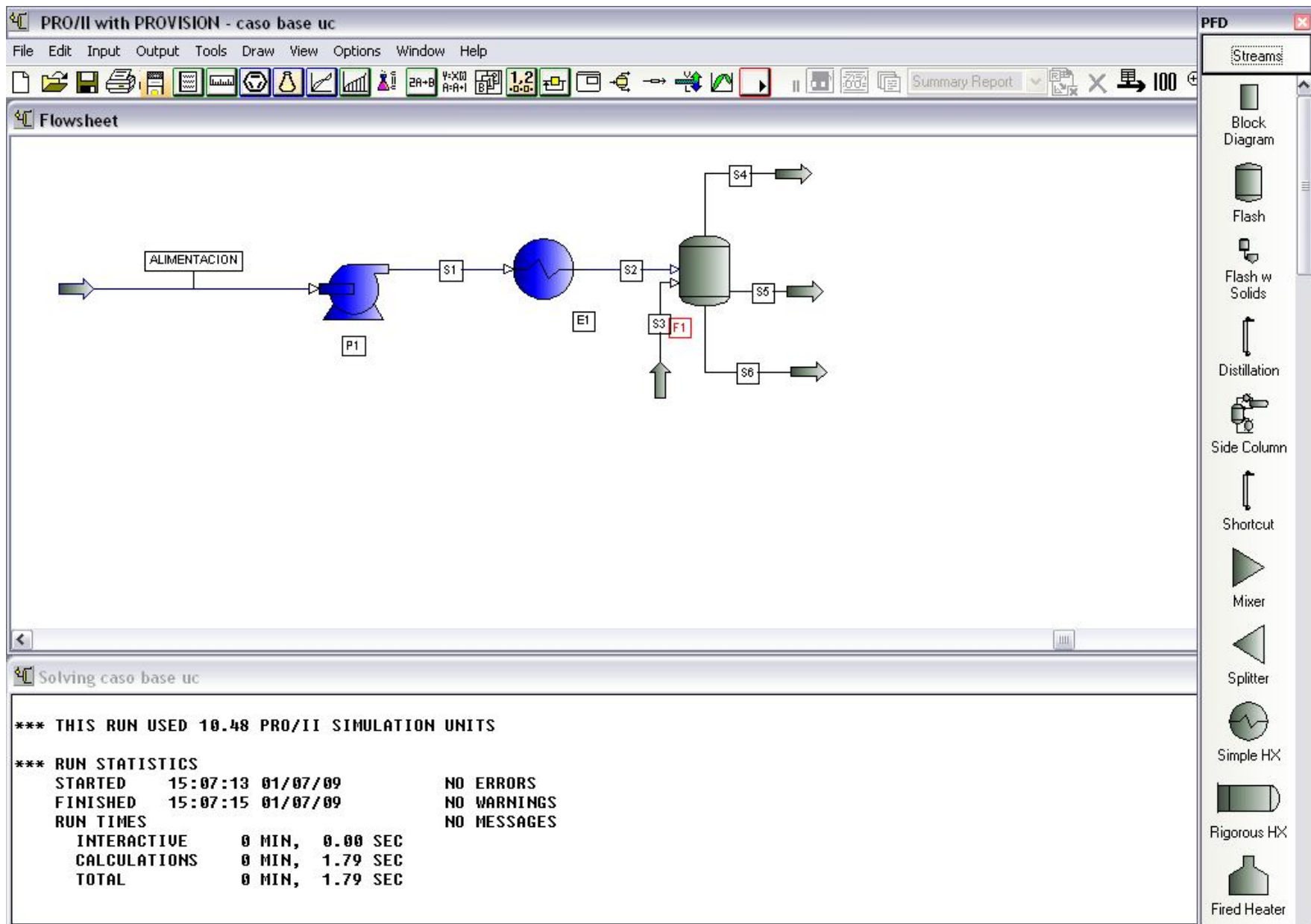
- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

Solving caso base uc

*** THIS RUN USED 10.48 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:07:13	01/07/09	NO ERRORS
FINISHED	15:07:15	01/07/09	NO WARNINGS
RUN TIMES			NO MESSAGES
INTERACTIVE	0 MIN,	0.00 SEC	
CALCULATIONS	0 MIN,	1.79 SEC	
TOTAL	0 MIN,	1.79 SEC	



PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Flash Drum

Unit: F1 Description:

First Specification: Pressure Drop 0.00000 psi Thermodynamic System: Default (SRKS01)

Second Specification: Unit Specification: Temperature Duty Dew Point Bubble Point Isentropic

Temperature Estimate: F Pressure Estimate: psia Pseudostream Flowrate: 0.00000 lb-mol/hr Phase Assignment: Default

Product Phases... Print Options... Entrainment...

OK Cancel

Select the unit specification

*** THIS RUN USED 10.48 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:07:13	01/07/09	NO ERRORS
FINISHED	15:07:15	01/07/09	NO WARNINGS
RUN TIMES			NO MESSAGES
INTERACTIVE	0 MIN,	0.00 SEC	
CALCULATIONS	0 MIN,	1.79 SEC	
TOTAL	0 MIN,	1.79 SEC	

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

PRO/II - Flash Drum

UOM Define Range Help Overview Status Notes

Unit: Description:

First Specification
 psi Thermodynamic System:

Second Specification
☒ Unit Specification: x 10⁶ BTU/hr
☐ Product Specification:
Parameter = value within the default tolerance

Temperature Estimate: F
Pressure Estimate: psia
Pseudostream Flowrate: lb-mol/hr
Phase Assignment:

Enter the duty

*** THIS RUN USED 10.48 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:07:13	01/07/09	NO ERRORS
FINISHED	15:07:15	01/07/09	NO WARNINGS
RUN TIMES			NO MESSAGES
INTERACTIVE	0 MIN,	0.00 SEC	
CALCULATIONS	0 MIN,	1.79 SEC	
TOTAL	0 MIN,	1.79 SEC	

PFD

Streams

- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

Flowsheet

Streams

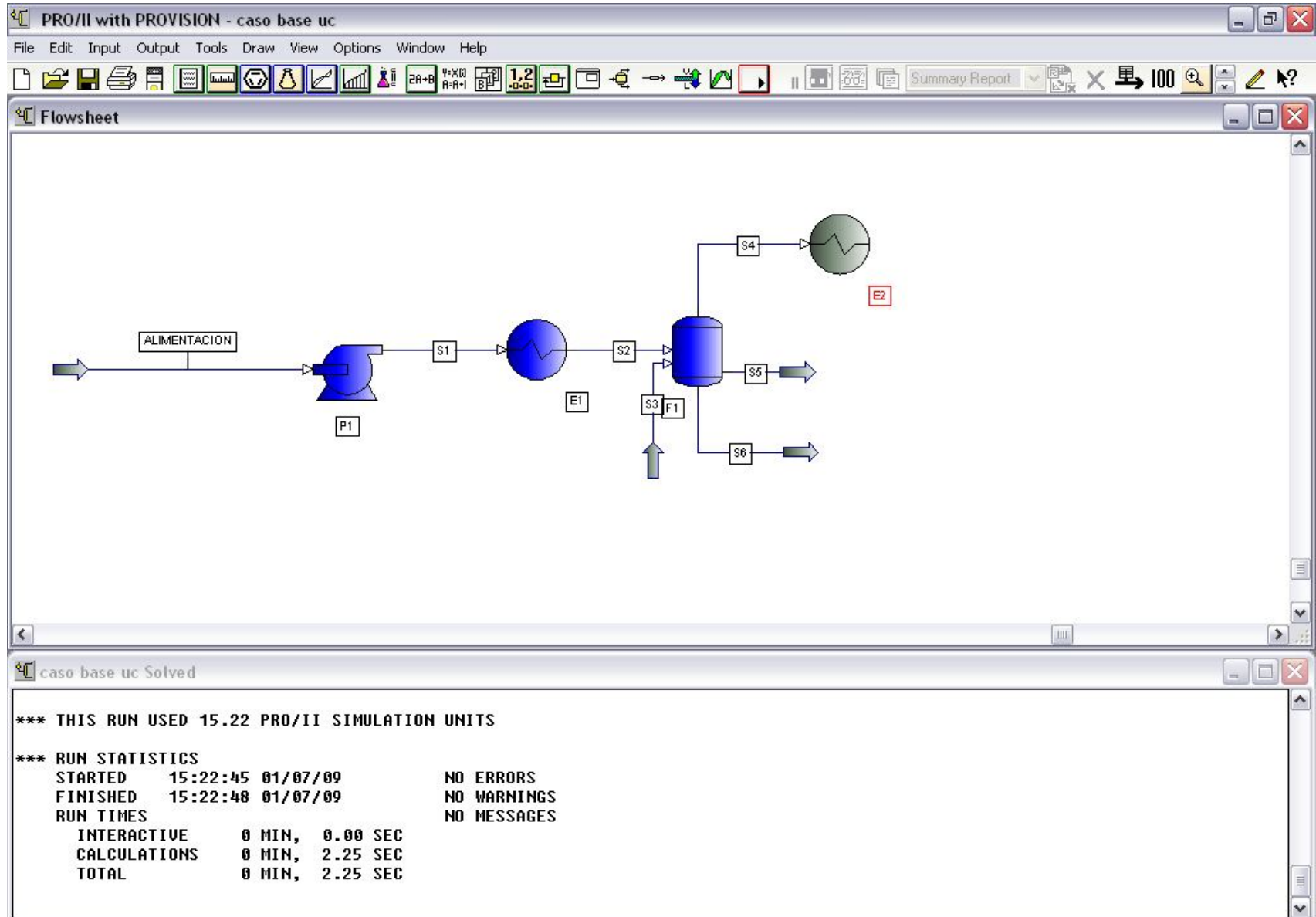
- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

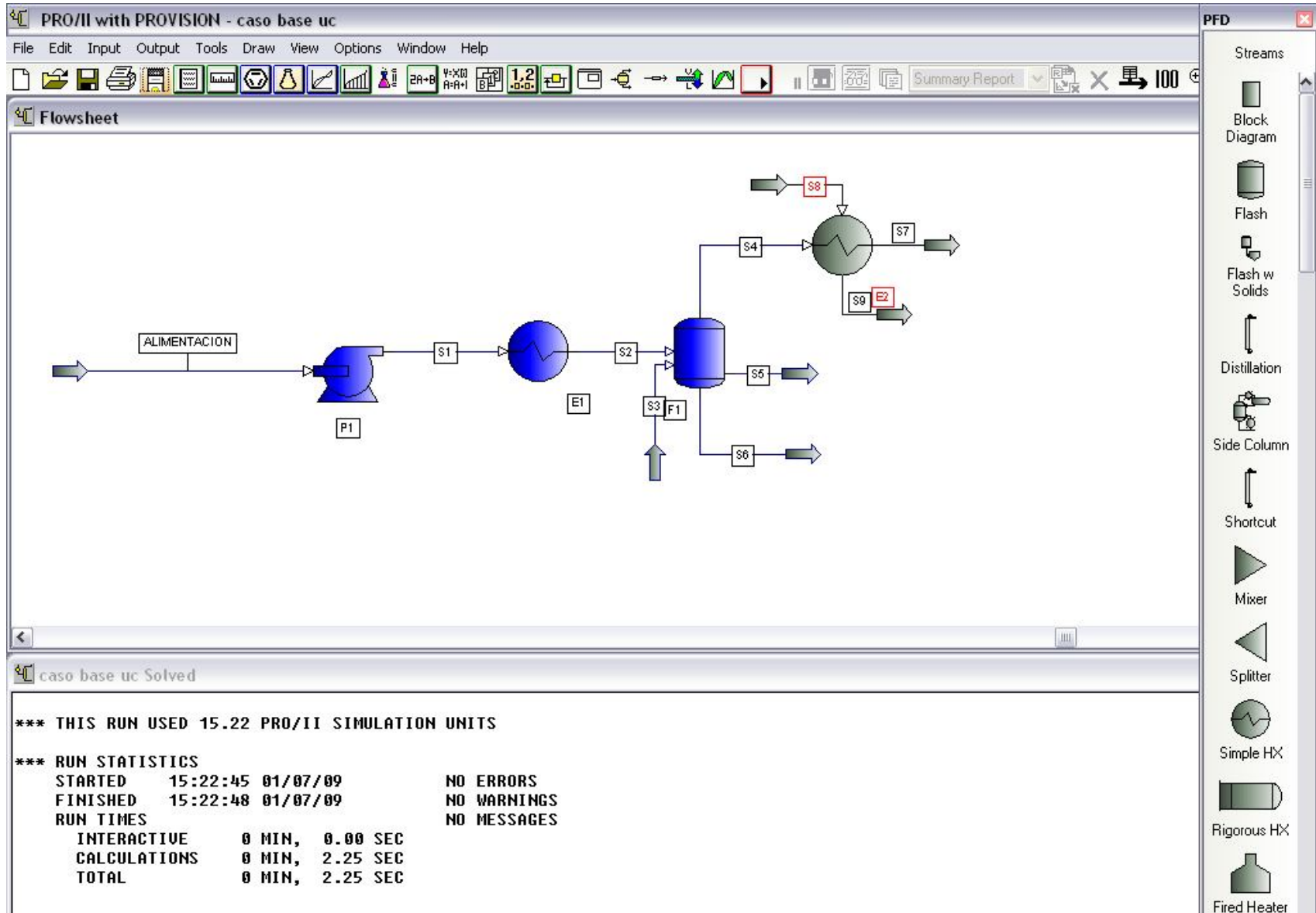
caso base uc Solved

*** THIS RUN USED 15.22 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:22:45	01/07/09	NO ERRORS
FINISHED	15:22:48	01/07/09	NO WARNINGS
RUN TIMES			NO MESSAGES
INTERACTIVE	0 MIN,	0.00 SEC	
CALCULATIONS	0 MIN,	2.25 SEC	
TOTAL	0 MIN,	2.25 SEC	





PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Heat Exchanger

Heat Exchanger - Process Streams

UOM Define Range Help

Specify Information for
☒ Hot ☐ Cold Product Phases...

Feeds: S4 Products: S7

Specify Information for
☐ Hot ☒ Cold Product Phases...

Feeds: S8 Products: S9

Specification...
Configuration...
Zones Analysis...
Print Options...

OK
Cancel

Exit the window after saving all data

Summary Report

100

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

caso base uc Solved

*** THIS RUN USED 15.22 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:22:45	01/07/09	NO ERRORS
FINISHED	15:22:48	01/07/09	NO WARNINGS
RUN TIMES			NO MESSAGES
INTERACTIVE	0 MIN,	0.00 SEC	
CALCULATIONS	0 MIN,	2.25 SEC	
TOTAL	0 MIN,	2.25 SEC	

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Heat Exchanger

UOM Define Range Help Overview Status Notes

Unit: E2 Description:

Hot Side

Process Stream...
Utility Stream...
Attach to Column...

Pressure Drop: 12.000 psi

Thermodynamic System: Default (SRKS01)

Cold Side

Process Stream...
Utility Stream...
Attach to Column...

Pressure Drop: 12 psi

Thermodynamic System: Default (SRKS01)

Specification...
Configuration...
Zones Analysis...
Print Options...

OK
Cancel

Enter the cold side pressure drop value

Summary Report

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

caso base uc Solved

*** THIS RUN USED 15.22 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED 15:22:45 01/07/09 NO ERRORS

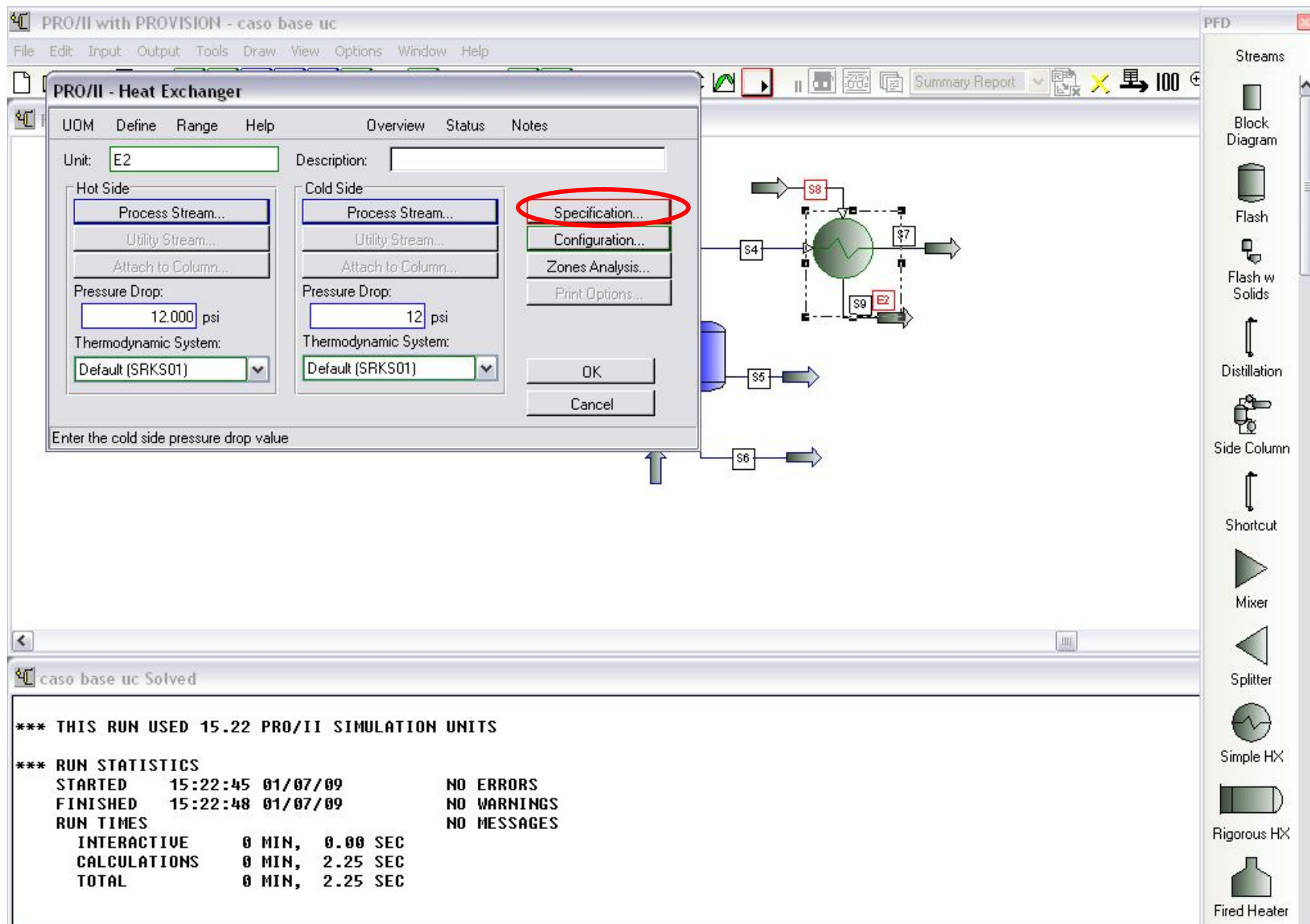
FINISHED 15:22:48 01/07/09 NO WARNINGS

RUN TIMES NO MESSAGES

INTERACTIVE 0 MIN, 0.00 SEC

CALCULATIONS 0 MIN, 2.25 SEC

TOTAL 0 MIN, 2.25 SEC



PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Heat Exchanger

Heat Exchanger - Specifications

UOM Define Range Help

Specification:

Relative Tolerance:

Area:

U-Value:

Maximum Allowable:

Select the specification:

- Area * U-value (Lumped Product)
- Area and U-value (Separate Values for Each)
- Cold Product Liquid Fraction
- Cold Product Temperature
- Cold Product Temperature Drop Below Bubble Point
- Cold Product Temperature Rise Above Dew Point
- Duty (Overall Exchanger)
- Hot Inlet - Cold Outlet Temperature Approach
- Hot Outlet - Cold Inlet Temperature Approach
- Hot Outlet - Cold Outlet Temperature Approach
- Hot Product Liquid Fraction
- Hot Product Temperature
- Hot Product Temperature Drop Below Bubble Point
- Hot Product Temperature Rise Above Dew Point
- Minimum Internal Temperature Approach
- Minimum of (Hot Out - Cold In) and (Hot In - Cold Out)

Summary Report

100

caso base uc Solved

*** THIS RUN USED 15.22 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:22:45	01/07/09	NO ERRORS
FINISHED	15:22:48	01/07/09	NO WARNINGS
RUN TIMES			NO MESSAGES
INTERACTIVE	0 MIN,	0.00 SEC	
CALCULATIONS	0 MIN,	2.25 SEC	
TOTAL	0 MIN,	2.25 SEC	

Streams

- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Heat Exchanger

Heat Exchanger - Specifications

UDM Define Range Help

Specification: Hot Product Liquid Fraction

Value: 0.8

Relative Tolerance: 0.000100

Area: ft²

U-Value: BTU/hr-ft²-F

Maximum Allowable U*A: BTU/hr-F

OK Cancel

Enter the specification value

PFD

Streams

- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

caso base uc Solved

*** THIS RUN USED 15.22 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:22:45	01/07/09	NO ERRORS
FINISHED	15:22:48	01/07/09	NO WARNINGS
RUN TIMES			NO MESSAGES
INTERACTIVE	0 MIN,	0.00 SEC	
CALCULATIONS	0 MIN,	2.25 SEC	
TOTAL	0 MIN,	2.25 SEC	

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Heat Exchanger

Unit:
Description:

Hot Side

Process Stream...

Utility Stream...

Attach to Column...

Pressure Drop: psi

Thermodynamic System:

Cold Side

Process Stream...

Utility Stream...

Attach to Column...

Pressure Drop: psi

Thermodynamic System:

Specification...

Configuration...

Zones Analysis...

Print Options...

OK

Cancel

Push to provide operating specification

caso base uc Solved

*** THIS RUN USED 15.22 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED 15:22:45 01/07/09 NO ERRORS

FINISHED 15:22:48 01/07/09 NO WARNINGS

RUN TIMES NO MESSAGES

INTERACTIVE 0 MIN, 0.00 SEC

CALCULATIONS 0 MIN, 2.25 SEC

TOTAL 0 MIN, 2.25 SEC

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Stream Data

UDM Range Help Tag Overview Status Notes

Stream: S8 Description:

To Unit: E2

Stream Type

- Composition Defined
- Petroleum Assay
- Referenced to Stream
- Solids Only Stream
- Flowrate and Composition...**
- Stream Solids Data...
- Stream Polymer Data...

Thermal Condition

First Specification:

Second Specification:

Thermodynamic System: Determined From Connectivity

OK Cancel

Push to bring up the flowrate and assay window

PFD

Streams

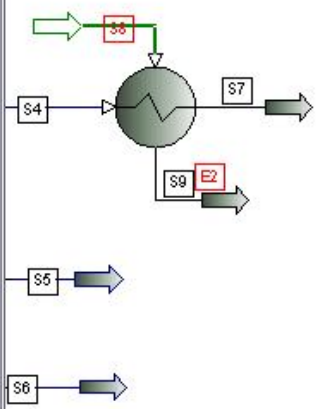
- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

caso base uc Solved

*** THIS RUN USED 15.22 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:22:45	01/07/09	NO ERRORS
FINISHED	15:22:48	01/07/09	NO WARNINGS
RUN TIMES			NO MESSAGES
INTERACTIVE	0 MIN,	0.00 SEC	
CALCULATIONS	0 MIN,	2.25 SEC	
TOTAL	0 MIN,	2.25 SEC	



PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Stream Data

Stream Data - Flowrate and Composition

UOM Range Help Tag

Specify flowrate and composition for stream S8

Fluid Flowrate Specification:

☒ Total Fluid Flowrate: 4000.0 lb-mol/hr

☐ Individual Component Flowrates

Copy	Component	Composition Mole
Paste	H2O	1
	NBP 389	
	NBP 412	
	NBP 437	
	NBP 462	
	NBP 487	
	NBP 513	

Clear Compositions Total: 0.00000 ☐ Normalize Component Flowrates Based on Specified Fluid Flowrate

OK Cancel

Enter the composition

Streams

- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

caso base uc Solved

*** THIS RUN USED 15.22 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED 15:22:45 01/07/09 NO ERRORS

FINISHED 15:22:48 01/07/09 NO WARNINGS

RUN TIMES

INTERACTIVE 0 MIN, 0.00 SEC

CALCULATIONS 0 MIN, 2.25 SEC

TOTAL 0 MIN, 2.25 SEC

NO MESSAGES

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

PRO/II - Stream Data

UQM Range Help Tag Overview Status Notes

Stream: S8 Description:

To Unit: E2

Stream Type

- Composition Defined
- Petroleum Assay
- Referenced to Stream
- Solids Only Stream

Flowrate and Composition...

Stream Solids Data...

Stream Polymer Data...

Thermal Condition

First Specification:

Temperature 66.00 F

Second Specification:

Pressure 214.7 psia

Thermodynamic System: Determined From Connectivity

OK Cancel

Enter stream pressure

Summary Report

100

Streams

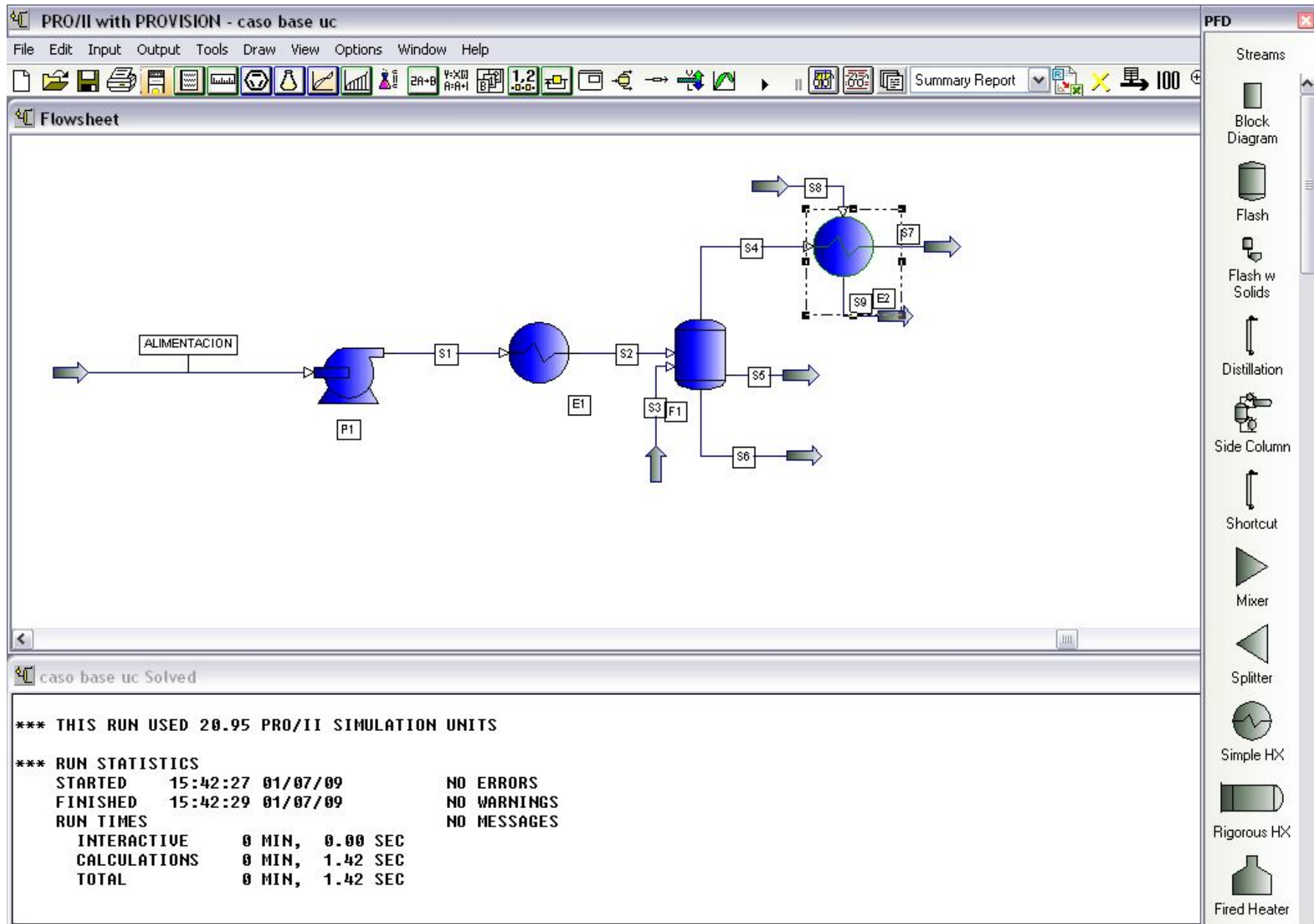
- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

caso base uc Solved

*** THIS RUN USED 15.22 PRO/II SIMULATION UNITS

*** RUN STATISTICS

Item	Value	Errors/Warnings/Messages
STARTED	15:22:45 01/07/09	NO ERRORS
FINISHED	15:22:48 01/07/09	NO WARNINGS
RUN TIMES		NO MESSAGES
INTERACTIVE	0 MIN, 0.00 SEC	
CALCULATIONS	0 MIN, 2.25 SEC	
TOTAL	0 MIN, 2.25 SEC	



PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

Summary Report 100

Flowsheet

ALIMENTACION

P1

E1

F1

S1, S2, S3, S4, S5, S6, S7, S8, S9

Context Menu:

- Data Review Window
- View Results
- View Excel Results
- Data Entry...
- Notes...
- Copy
- Collapse
- Delete
- Rotate
- Flip
- Restore Label Position
- Center in View
- Center Upstream Unit
- Reroute
- Display...
- Rename...
- Add to Active Report

Solving caso base uc

*** THIS RUN USED 20.95 PRO/II SIMULATION UNITS

*** RUN STATISTICS

STARTED	15:42:27	01/07/09	NO ERRORS
FINISHED	15:42:29	01/07/09	NO WARNINGS
RUN TIMES			NO MESSAGES
INTERACTIVE	0 MIN,	0.00 SEC	
CALCULATIONS	0 MIN,	1.42 SEC	
TOTAL	0 MIN,	1.42 SEC	

PFD

- Streams
- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

Programmer's File Editor

File Edit Options Template Execute Macro Window Help

Documents and Settings\miajaa\Configuración local\Temp\VW185.tmp

STREAM 'S7'

	TOTAL	VAPOR	LIQUID 1	LIQUID 2
RATE, LB-MOL/HR	2283.9766	456.7950	4.3091	1822.8726
TEMPERATURE, F	383.43	383.43	383.43	383.43
PRESSURE, PSIA	206.70	206.70	206.70	206.70
MOLECULAR WEIGHT	18.8548	20.6723	181.2409	18.0155
FRACTION		0.2000	1.8867E-03	0.7981
ENTHALPY, BTU/LB-MOL	9721.8152	22455.0416	32448.0343	6477.2643
CP, BTU/LB-F	0.9422	0.4997	0.5807	1.0780

MOLAR FLOWRATES, LB-MOL/HR

1 - H2O	2273.0212	449.1506	1.0014	1822.8693
2 - NBP 389	1.8548	1.7018	0.1517	1.3485E-03
3 - NBP 412	1.7611	1.5750	0.1852	9.2538E-04
4 - NBP 437	1.3387	1.1530	0.1852	4.8597E-04
5 - NBP 462	1.0289	0.8416	0.1870	2.5273E-04
6 - NBP 487	0.8393	0.6397	0.1994	1.3599E-04
7 - NBP 513	0.7589	0.5260	0.2329	7.8894E-05
8 - NBP 538	0.7067	0.4322	0.2744	4.5791E-05
9 - NBP 562	0.5889	0.3068	0.2820	2.3031E-05
10 - NBP 587	0.4173	0.1776	0.2397	9.4373E-06

*** I

Ln 1 Col 1 76 WR Rec Off No Wrap DOS INS NUM

*** RUN STATISTICS

STARTED 15:42:27 01/07/09 NO ERRORS

FINISHED 15:42:29 01/07/09 NO WARNINGS

RUN TIMES NO MESSAGES

INTERACTIVE 0 MIN, 0.00 SEC

CALCULATIONS 0 MIN, 1.42 SEC

TOTAL 0 MIN, 1.42 SEC

PFD

Streams

Block Diagram

Flash

Flash w Solids

Distillation

Side Column

Shortcut

Mixer

Splitter

Simple HX

Rigorous HX

Fired Heater

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

Programmer's File Editor - [V:\Documents and Settings\miajaa\Configuración local\Temp\VW187.tmp]

File Edit Options Template Execute Macro Window Help

STREAM 'S9'

	TOTAL	VAPOR
RATE, LB-MOL/HR	4000.0000	4000.0000
TEMPERATURE, F	388.18	388.18
PRESSURE, PSIA	214.70	214.70
MOLECULAR WEIGHT	18.0153	18.0153
FRACTION		1.0000
ENTHALPY, BTU/LB-MOL	22039.1250	22039.1250
CP, BTU/LB-F	0.4992	0.4992

MOLAR FLOWRATES, LB-MOL/HR

1 - H2O	4000.0000	4000.0000
2 - NBP 389	0.0000	0.0000
3 - NBP 412	0.0000	0.0000
4 - NBP 437	0.0000	0.0000
5 - NBP 462	0.0000	0.0000
6 - NBP 487	0.0000	0.0000
7 - NBP 513	0.0000	0.0000
8 - NBP 538	0.0000	0.0000
9 - NBP 562	0.0000	0.0000
10 - NBP 587	0.0000	0.0000
11 - NBP 612	0.0000	0.0000
12 - NBP 640	0.0000	0.0000
13 - NBP 660	0.0000	0.0000

*** RUN STATISTICS

STARTED 15:42:27 01/07/09 NO ERRORS

FINISHED 15:42:29 01/07/09 NO WARNINGS

RUN TIMES NO MESSAGES

INTERACTIVE 0 MIN, 0.00 SEC

CALCULATIONS 0 MIN, 1.42 SEC

TOTAL 0 MIN, 1.42 SEC

Streams

- Block Diagram
- Flash
- Flash w Solids
- Distillation
- Side Column
- Shortcut
- Mixer
- Splitter
- Simple HX
- Rigorous HX
- Fired Heater

PRO/II with PROVISION - caso base uc

File Edit Input Output Tools Draw View Options Window Help

Programmer's File Editor

File Edit Options Template Execute Macro Window Help

Documents and Settings\miajaa\Configuración local\Temp\VW18B.tmp

Heat Exchanger 'E1'

Feeds - Cold Side S1
Products - Cold Side S2

	User Input	Calculated
Hot Pressure Drop, PSI		0.00
Cold Outlet Temperature, F	662.00	662.00
Cold Pressure Drop, PSI	8.00	8.00
Cold Liquid Fraction		1.0000
Duty, MM BTU/HR		66.3554

Ln 1 Col 1 15 WR Rec Off No Wrap DOS INS NUM

*** RUN STATISTICS

STARTED	15:42:27 01/07/09	NO ERRORS
FINISHED	15:42:29 01/07/09	NO WARNINGS
RUN TIMES		NO MESSAGES
INTERACTIVE	0 MIN, 0.00 SEC	
CALCULATIONS	0 MIN, 1.42 SEC	
TOTAL	0 MIN, 1.42 SEC	